

City of Pasadena
Department of Water and Power

ADDENDUM NO. 2
to

Specifications LD-13-14
for

PROVIDING LABOR AND MATERIALS FOR
GLENARM REPOWERING BALANCE OF PLANT DESIGN AND CONSTRUCTION

This addendum is issued to correct and clarify the above Specifications. All addenda will be issued electronically. This addendum shall be considered in the bid proposal and become a part of any contract made pursuant thereto:

1. Replace the following documents within Attachment A.2 of the Specification. See Enclosure 1.
 - Ammonia System P&ID, Dwgs SKM1-8 Rev A & SKM1-9 Rev A with the drawing SKM1-8 Rev B & SKM1-9 Rev B accordingly.
 - General Arrangement, Dwg M1-1-1 Rev K with M1-1-1 Rev L.
 - PDC Layout, Dwg E1-2 Rev D with E1-2 Rev E in Section 260533 (Non Segregated-Phase Bus and Section 261200-2 (Medium Voltage Auxiliary Transformers).
 - Electrical One-Line, Dwg E1-1A Rev E with E1-1A Rev G in Section 260533 (Non Segregated-Phase Bus and .Section 261200-2 (Medium Voltage Auxiliary Transformers).
 - Tie Points, Dwg M1-1-6 Rev D with M1-1-6 Rev E.
2. Enclosure 2 is not used.

3. Add the following documents to the Attachment A.3 of the Specification. See Enclosure 3.
 - Topographic Survey Dwgs TP-1, TP-2, & TP-3.
 - Shin Nippon Steam Turbine Steam Quality Requirements
 - IST Engineering Specification – Feedwater Quality Requirements for Superheated Steam Applications – Specification No ES-1000 Rev 9.
 - IST Jumper Tube Installation Proposal – P12079-00 Jumper Tubes.
 - Prolec GSU Transformer Preliminary Proposal Dwg 221732C1.
 - Prolec GSU Transformer Technical Proposal Information Form 3.2.1-D Rev.0.
 - SPX Cooling Technologies Preliminary Dwg No. JV4688445 – Schematic View.
 - SPX Cooling Technologies Preliminary Dwg No. JV468844B – Basin Plan View.
 - SPX Cooling Technologies Preliminary Dwg No. JV468844D – Basin Section & Details.
 - Holtec Steam Surface Condenser Dwg SK-8371-0 Rev 0.
 - Shin Nippon Steam Turbine Foundation Dwg Sheets 1of4 and 2of4.
 - Shin Nippon Steam Turbine Layout Dwg 11415-0002-10 Rev 6.
 - Shin Nippon Steam Turbine Foundation Loading Data.
 - Hyundai IDEAL Steam Turbine Generator Outline Dwg 5065A0-23 Rev F.
 - Hyundai IDEAL Aftermarket Service Bulletin Dated 03-01-08.
4. Add the following documents from the January 8, 2014 Pre-Bid Meeting and Job Walk as part of the Specifications. See Enclosure 4.
 - BOP Contractor Pre-Bid Meeting Introduction
 - BOP RFP Pre-Bid Presentation
 - BOP Contractor Pre-Bid Meeting Outreach
 - IST Glenarm Repowering Project OTSG Erection
 - GE Power Island Equipment Review
 - GE LM 6000 Package Evolution.
 - Pre-Bid Meeting Sign Up Sheet
5. Add the following City of Pasadena Department of Public Works Permit Requirement Documents as part of the Specifications. See Enclosure 5.
 - Construction Staging and Traffic Management Plan – Template.
 - Construction Staging & Traffic Management Plan – Truck Routes.
 - Contracts/Purchase Orders/Permits Insurance Requirements.
 - City of Pasadena Dept of Public Works Permit Location and Working Hours.
 - Moving Permit Application – For Wide Load & Heavy Equipment.
 - City of Pasadena Application For a Permit to Conduct an Activity within the Public Right-of-Way.
 - City of Pasadena Proposed Storage Container Guideline – Street Occupation.

- City of Pasadena – Department of Public Works Application for a Permit to Place a Storage Container in Public Right of Way.
 - City of Pasadena FY 2014 Adopted General Fee Schedule Part 2.
6. Replace Attachments A.2 Document List and A.3 Reference Document List of the Specification with the versions included in Enclosure 6.
 7. Add the Q & A Table Rev 0 as part of the Specifications. See Enclosure 7.
 8. CAD files for the General Arrangement, Site Plan, and Grading Plan were sent to the following individuals

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ARB

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Bob Anders – bob.anders@worleyparsons.com

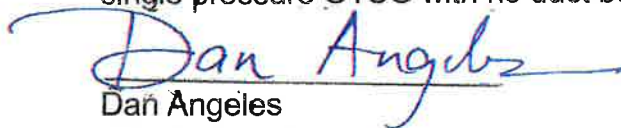
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WoodGroup

John Smith – [jk.smith@woodgroup.com](mailto:j.k.smith@woodgroup.com)
Ray Stankowski – stankowski@pbworld.com

9. IST's drawing ED-002 "Generic Flowsheet Dual Pressure OTSG w/ Burner, SCR, CO) is included within various IST documents such as their presentation at the Pre-Bid meeting. This drawing is included for illustrative purposes only and the specific IST drawing for this project should be used. To clarify further, this project utilizes a single pressure OTSG with no duct burning.



Dan Angeles
Principal Engineer
City of Pasadena Water and Power Department

Date: 1/16/14

Enclosures: Enclosure 1
Enclosure 2
Enclosure 3
Enclosure 4
Enclosure 5
Enclosure 6
Enclosure 7

RECEIPT OF ADDENDUM NO. 2

Specifications LD-13-14

**for
PROVIDING LABOR AND MATERIALS FOR
GLENARM REPOWERING BALANCE OF PLANT DESIGN AND CONSTRUCTION
FOR
PASADENA WATER & POWER
PASADENA, CALIFORNIA**

This Receipt must be signed and returned with your bid. Failure to include signed acknowledgements of all addenda will cause the bid to be deemed incomplete and nonresponsive.

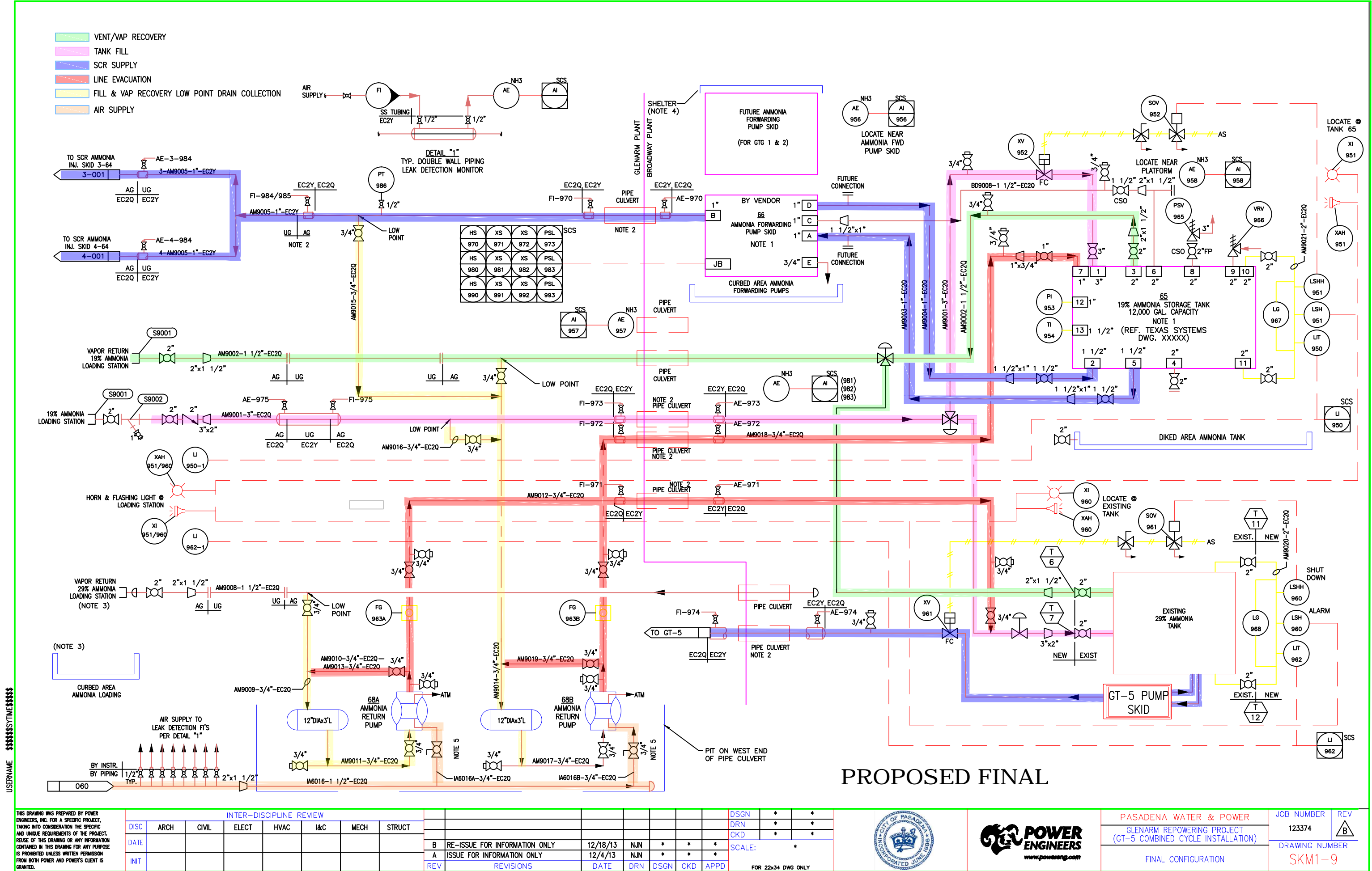
I hereby acknowledge receipt of Addendum No. 2 for Specifications LD-13-14 for Providing Labor and Materials for Glenarm Repowering Balance of Plant Design and Construction.

Date

Company Name

Authorized Signature

Enclosure 1



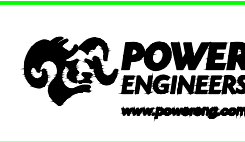
PROPOSED FINAL

THIS DRAWING WAS PREPARED BY POWER ENGINEERS, INC. FOR A SPECIFIC PROJECT, TAKING INTO CONSIDERATION THE SPECIFIC AND UNIQUE REQUIREMENTS OF THE PROJECT. REUSE OF THIS DRAWING OR ANY INFORMATION CONTAINED IN THIS DRAWING FOR ANY PURPOSE IS PROHIBITED UNLESS WRITTEN PERMISSION FROM BOTH POWER AND POWER'S CLIENT IS GRANTED.

INTER-DISCIPLINE REVIEW							
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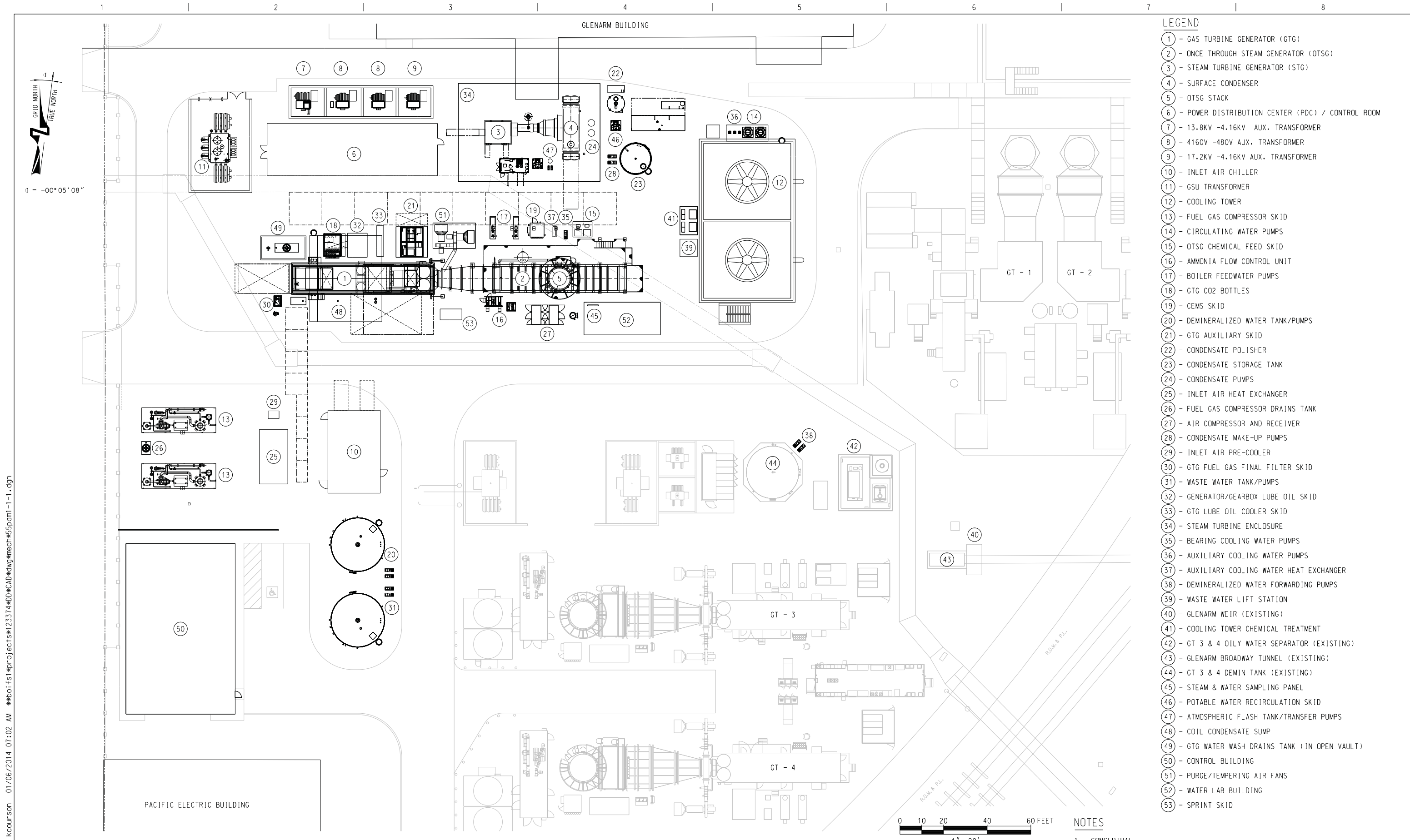
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B	RE-ISSUE FOR INFORMATION ONLY	12/18/13	NJN	*	*	*
A	ISSUE FOR INFORMATION ONLY	12/4/13	NJN	*	*	*

DSGN	*	*
DRN	*	*
CKD	*	*
SCALE:	*	
FOR 22x34 DWG ONLY		






PASADENA WATER & POWER
GLENARM REPOWERING PROJECT
(GT-5 COMBINED CYCLE INSTALLATION)
FINAL CONFIGURATION

JOB NUMBER	REV
123374	B
DRAWING NUMBER	
SKM1-9	

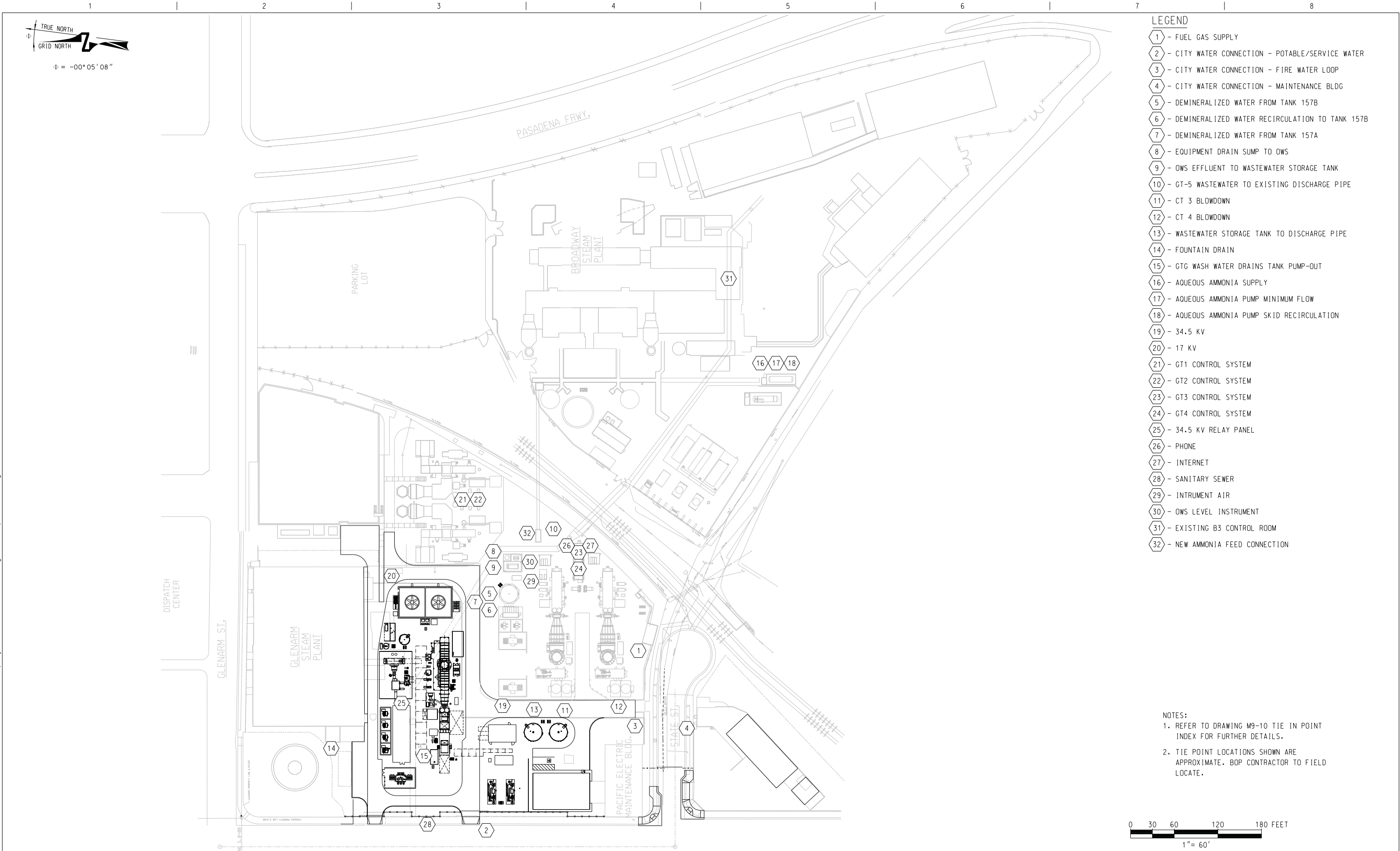


- LEGEND**
- 1 - GAS TURBINE GENERATOR (GTG)
 - 2 - ONCE THROUGH STEAM GENERATOR (OTSG)
 - 3 - STEAM TURBINE GENERATOR (STG)
 - 4 - SURFACE CONDENSER
 - 5 - OTSG STACK
 - 6 - POWER DISTRIBUTION CENTER (PDC) / CONTROL ROOM
 - 7 - 13.8KV -4.16KV AUX. TRANSFORMER
 - 8 - 4160V -480V AUX. TRANSFORMER
 - 9 - 17.2KV -4.16KV AUX. TRANSFORMER
 - 10 - INLET AIR CHILLER
 - 11 - GSU TRANSFORMER
 - 12 - COOLING TOWER
 - 13 - FUEL GAS COMPRESSOR SKID
 - 14 - CIRCULATING WATER PUMPS
 - 15 - OTSG CHEMICAL FEED SKID
 - 16 - AMMONIA FLOW CONTROL UNIT
 - 17 - BOILER FEEDWATER PUMPS
 - 18 - GTG CO2 BOTTLES
 - 19 - CEMS SKID
 - 20 - DEMINERALIZED WATER TANK/PUMPS
 - 21 - GTG AUXILIARY SKID
 - 22 - CONDENSATE POLISHER
 - 23 - CONDENSATE STORAGE TANK
 - 24 - CONDENSATE PUMPS
 - 25 - INLET AIR HEAT EXCHANGER
 - 26 - FUEL GAS COMPRESSOR DRAINS TANK
 - 27 - AIR COMPRESSOR AND RECEIVER
 - 28 - CONDENSATE MAKE-UP PUMPS
 - 29 - INLET AIR PRE-COOLER
 - 30 - GTG FUEL GAS FINAL FILTER SKID
 - 31 - WASTE WATER TANK/PUMPS
 - 32 - GENERATOR/GEARBOX LUBE OIL SKID
 - 33 - GTG LUBE OIL COOLER SKID
 - 34 - STEAM TURBINE ENCLOSURE
 - 35 - BEARING COOLING WATER PUMPS
 - 36 - AUXILIARY COOLING WATER PUMPS
 - 37 - AUXILIARY COOLING WATER HEAT EXCHANGER
 - 38 - DEMINERALIZED WATER FORWARDING PUMPS
 - 39 - WASTE WATER LIFT STATION
 - 40 - GLENARM WEIR (EXISTING)
 - 41 - COOLING TOWER CHEMICAL TREATMENT
 - 42 - GT 3 & 4 OILY WATER SEPARATOR (EXISTING)
 - 43 - GLENARM BROADWAY TUNNEL (EXISTING)
 - 44 - GT 3 & 4 DEMIN TANK (EXISTING)
 - 45 - STEAM & WATER SAMPLING PANEL
 - 46 - POTABLE WATER RECIRCULATION SKID
 - 47 - ATMOSPHERIC FLASH TANK/TRANSFER PUMPS
 - 48 - COIL CONDENSATE SUMP
 - 49 - GTG WATER WASH DRAINS TANK (IN OPEN VAULT)
 - 50 - CONTROL BUILDING
 - 51 - PURGE/TEMPERING AIR FANS
 - 52 - WATER LAB BUILDING
 - 53 - SPRINT SKID

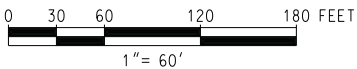
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										DATE								I	RE-ISSUED FOR BID				10/15/2013	VBD	KAC	TRC	GTH	CKD	RVK	04/12/2011			GENERAL ARRANGEMENT GAS TURBINE/AXIAL EXHAUST		DRAWING NUMBER	
										INIT								H	RE-ISSUED FOR REVIEW				09/27/2013	VBD	KAC	ADD	SLH	SCALE: 1" = 20'-0"								
																		REV	REVISIONS				07/18/2013	VBD	KAC	ADD	SLH	FOR 22x34 DWG ONLY								

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- NOTES:
1. REFER TO DRAWING M9-10 TIE IN POINT INDEX FOR FURTHER DETAILS.
 2. TIE POINT LOCATIONS SHOWN ARE APPROXIMATE. BOP CONTRACTOR TO FIELD LOCATE.



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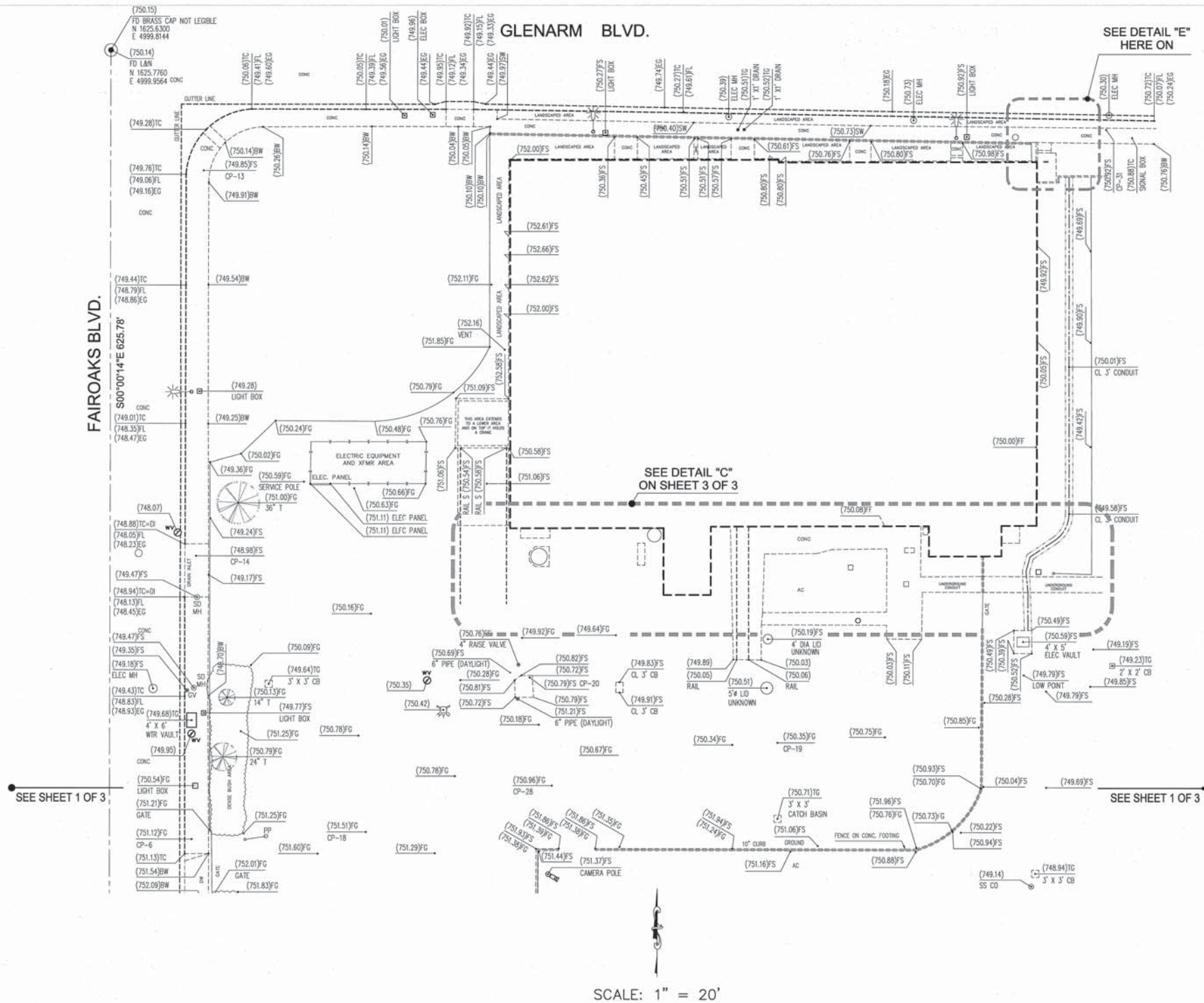
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REV	REVISIONS	DATE	DRN	DSGN	CKD	APPD			



PASADENA WATER & POWER		JOB NUMBER	REV
GLENARM REPOWERING PROJECT (GT-5 COMBINED CYCLE INSTALLATION)		123374	E
TIE POINT DRAWING GAS TURBINE/AXIAL EXHAUST		DRAWING NUMBER	
		M1-1-6	

Enclosure 2 (Not Used)

Enclosure 3



SCALE: 1" = 20'



CIVIL ENGINEERING & LAND SURVEYING
COORY ENGINEERING
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1718 N. NEVILLE STREET, ORANGE, CA 92865

TOPOGRAPHIC SURVEY
PASADENA GLENARM FACILITY

PASADENA, CA

PREPARED FOR: PASADENA WATER AND POWER

DRAWN BY: SAS SCALE: 1" = 20' SHEET: 2 of 3 TP-2

CHECKED BY: SMK JOB NO: 505-101

DISREGARD PRINTS BEARING
EARLIER REVISION DATES → 04-04-11

REVISIONS				
NO	DESCRIPTION	BY	APPROVED	DATE

14. STEAM QUALITY

Deposits on the turbine blading due to steam contamination may bring about thermodynamical and mechanical disturbances. Moreover, if chlorides are involved under certain circumstances blade fractures might occur.

Corrosion depending strain, caused by aggressive deposits, affects above all in the state of commencing steam wetness the alternating bending strength of the blade material.

These recommendations concerning the steam quality are in line with the guide lines for continuous turbine operation issued by the VGB (Vereinigung der Großkesselbetreiber in Deutschland).

On principle the guide lines should be complied with as far as practicable. The expenses for the relevant water treatment are to be seen in comparison with possible repair and stoppage costs if the turbine suffers damage from contaminated steam.

To avoid misunderstandings we point out that even full compliance with the guide lines does not guarantee absolutely safe a depositfree turbine. The steam contaminations and their portion of mixture represent the most essential factor as to precipitation, however, this problem is not fully solved up to now. If there is a chance to improve the steam cleanliness in comparison with the guide lines, make use of it.

Guide Lines for inlet steam condensate

Testing as to	Unit	Guide Lines	
		Continuous Operation +)	Start-up Operation ++)
Conductivity at 25°C for CO ₂ -free waters	μ S/cm	≤ 0.2	< 0.5
Silica (SiO ₂)	p.p.m	< 0.02	< 0.05
Total-iron (Fe)	p.p.m	< 0.02	< 0.05
Copper (Cu)	p.p.m	< 0.003	< 0.01
Sodium + Potassium (Na) (K)	p.p.m	< 0.01	< 0.02

+) The values are in line with the VGB-guide lines, edition April 1972. As to further details and descriptions see also there.

++) A falling tendency must be noticeable. On commissioning of new plants the values for continuous operation must be achieved after two days and the values for for start-up operation after two hours. Routine commissioning requires full compliance with the start-up values at the point of roll-off whereas the continuous operation values must be attained after 2 hours.

Supervision

Continuous monitoring of the water/steam system by means of recording instruments is recommended for the electrical conductivity at 25°C and for the Silica content. The monitoring instruments should be provided on the inlet steam or on the exhaust steam side.



ENGINEERING SPECIFICATION

Feedwater Quality Requirements for Superheated Steam Applications

SPECIFICATION NO. ES-1000

REVISION 09

simply generates more profit

Innovative Steam Technologies
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Revision Page

Revision Number	Description of Revision	Developed By	Approved By	Approval Date
01	General Revision	-----	-----	Sept 11/96
02	General Revision	-----	-----	Sept 23/96
03	Updated address to Conestoga Blvd	-----	-----	Nov 13/00
04	Revision of entire specification	-----	-----	April 3/02
05	Revision of oxygen levels Added Notes to Table 1 and Table 2	-----	-----	Sept 17/02
06	Added note (7) following cycle chemistry limits regarding pH values	-----	-----	Nov 20/02
07	Table 1.0, 2.0, Note (3) for Tables 1.0 and 2.0, Section 2.2	AB	JM	Aug 8/03
08	Format change update to new logo/font	SV		March 5/07
09	Removed specific conductivity	JM	CK	July 22/11

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1.0 INTRODUCTION

1.1 Background

This specification details the requirements of feedwater quality for Innovative Steam Technologies Once Through Steam Generators (OTSG's) producing superheated steam. Deviations from the limits and requirements must have specific written approval from Innovative Steam Technologies.

This specification addresses the following:

- all-volatile treatment (AVT) for applications with and without copper alloys in the pre-boiler and steam user systems
- oxygenated treatment for applications with all ferrous (no copper) pre-boiler systems

The technical criteria for formulating these guidelines includes:

- Avoidance of scale formation in the OTSG. Solids (dissolved or suspended) which are carried into the OTSG are either deposited in the tubing or carried through as a solid or vapour into the dry out zone where deposition may occur. Deposits may restrict flow as well as heat transfer and potentially act as corrosion sites.
- Suspended solids could end up plugging the stabilization orifices, which would restrict the flow to individual circuits.
- Prevention of corrosion and deposition in the OTSG. If necessary, more stringent limits can be used based on the requirements for other components in the system, which may be more sensitive to impurities.
- Generation of high purity steam

This specification is not a substitute for complete cycle chemistry guidelines, which should include monitoring of additional cycle streams as required. Successful implementation of this specification requires proper training of operators and is the responsibility of the owner.

1.2 Treatment Options

In once-through boilers, there are only two available options for water treatment, all volatile treatment (AVT) and oxygenated treatment (OT). Both treatments are feedwater treatments.

If copper alloys are used, OT cannot be used because the presence of oxygen accelerates copper alloy corrosion. If polishers are not to be used, or copper is present in the pre-boiler cycle, then AVT is the only option. With polishers and all ferrous pre-boiler metallurgy, either AVT or OT can be used.

Some of the chemicals referred to in this specification are hazardous to human health and/or environment and should be handled with care.

All-Volatile Treatment (AVT) is used to minimize corrosion and erosion corrosion in the pre-boiler system by using deaerated high purity water with an elevated pH. The pH elevation is achieved by the addition of ammonia. The target range for pH depends upon the metallurgy of the pre-boiler system (all-ferrous or Fe-Cu mixed). The oxygen concentration in the feedwater is reduced using an oxygen scavenger, such as hydrazine or carbohydrazide. The result of AVT treatment is a layer of magnetite (Fe_3O_4) on all steel surfaces which protects the metal from corrosion.

Oxygenated Treatment (OT) uses oxygenated high purity water to minimize corrosion and erosion-corrosion in the pre-boiler system. Oxygen, hydrogen peroxide, or air is injected into the feedwater to achieve an oxidizing environment. The pH is adjusted using ammonia, but the target pH range is lower than in AVT. IST has no operating experience to date with oxygenated treatment and as such IST has not

provided recommended feedwater limits for OT.

1.3 Makeup and Condensate Return Treatment

Raw water used for makeup contains impurities that must be removed before the water enters the OTSG. The extent of makeup water purification is system dependent (dependent on makeup rate) and site specific (dependent on raw water quality).

Condensate return water may contain impurities that must be removed before the water enters the OTSG. The extent of purification is system dependent (dependent on where steam is being used and how it is being contaminated).

1.4 Demineralizer and Polisher

The production of good quality feedwater is usually a function of a makeup demineralizer and a condensate polisher, although depending on system requirements, one of these items can sometimes be eliminated. Where demineralizer or polisher requirements are minimal, replacement resin bottles can minimize system capital and operating costs. This can eliminate the need for onsite acid and caustic facilities used for regeneration.

1.5 Organic Compounds

Precautions must be taken to eliminate organics prior to the water reaching the boiler since they can break down to acid type compounds at boiler operating temperatures. These acids can be harmful to the tubing of the OTSG and may have a negative affect on the feedwater treatment system resins.

Corrosion and flow-accelerated corrosion effects and removal of harmful decomposition products must be considered when selecting the type of feedwater treatment and the water treatment chemicals. Use of organic feedwater treatment chemicals (amines and oxygen scavengers) needs to be thoroughly evaluated concerning their decomposition, monitoring, analytical interferences, and toxicity.

Amines are not recommended for control of feedwater pH. They thermally decompose in the boiler and the steam circuits, forming organic acids, carbon dioxide, ammonia, and other decomposition products. This also happens to oxygen scavengers other than hydrazine. The harmful effects of some of the decomposition products may be reduced when condensate polishers are used. Hydrazine or carbohydrazide can be used for oxygen scavenging. Hydrazine is preferred since carbohydrazide decomposes forming acid species making it difficult to meet cation conductivity limits.

1.6 Control Parameters

The most important control parameter for the IST OTSG proper is feedwater cation conductivity. Dissolved oxygen and pH are to be continuously monitored to control corrosion in the pre-boiler system. Conductivity measurement is recommended because there is a direct correlation between dissolved solids and conductivity. The purpose of the cation conductivity measurement is to remove the masking effect of the ammonia/amines and its derivatives, in the water. Specific conductivity is not recommended and is not addressed in this specification.

ORP (oxidation reduction potential) is a method of grading a solution as oxidizing or reducing. The ORP value is a direct reading of the activity of the oxidizing and reducing agents in the water as they correspond to oxidation-reduction reactions. The oxidation-reduction reaction is an electrochemical process in which metal atoms are oxidized to form positive ions (cations) while other chemical species (O_2 , H_2O , H^+ and other cations) are reduced. This results in a flow of electrons from one site on the metal surface to another. For example, if the ORP is negative, a reducing environment exists that can reduce or eliminate a protective layer of magnetite.

Steam and feedwater conductivity measurements are both required to alert the operator of any components breaking down in the OTSG.

1.7 Chemical Feed Points

The chemical feed points for ammonia and the oxygen scavenger should be after the condensate polishers, since these compounds can be removed by the polisher. However, if the polishers are operated in the ammonia form, the ammonia addition can be at the exit of the condensate pumps. If there is a deaerator in the pre-boiler system, the best location to add the oxygen scavenger is into the drop leg of the deaerator. This allows a greater residence time of the scavenger in the feedwater, increasing its effectiveness.

1.8 Sample Points

To monitor the OTSG, it is recommended that sample points be located on the feedwater piping at the OTSG inlet and on the steam piping at the exit of the OTSG, after attemperating sprays (if installed). In cycles with reheat, hot reheat steam can be monitored instead.

It has been shown that for sampling of superheated steam, an isokinetic sampling nozzle is needed. Multi-port nozzles which are installed in the superheated steam piping are not isokinetic and do not give a representative sample. The same isokinetic sampling is needed when sampling feedwater for suspended oxides (Fe, Cu oxides) to ensure a representative sample.

When sampling cation conductivity a calibration check of the measuring instrument should be made using a standard solution of known value. If the reading is high, the measurement probe may need replacing.

2.0 CONTROL PARAMETERS AND LIMITS

2.1 Cycle Chemistry Limits

The rationale for determination of the cycle chemistry limits for these guidelines is based on the requirements for the OTSG. If necessary, more stringent limits can be used based on the requirements for other components in the system, which may be more sensitive to impurities.

The control limits to be used during normal operation are shown in Tables 1 and 2 for units on AVT. Oxygenated treatment (OT) is presently under investigation and limits have not been provided. These tables also include recommended monitoring frequencies and action levels, which allow exceeding the normal limits for short durations.

Parameter		Monitoring Frequency	Target Value	Action Level 1	Action Level 2	Action Level 3	Action Level 4
pH (see Note 7)	All ferrous	C	9.3 to 9.6	<9.3 or >9.6	-	-	-
	All stainless	C	8.0 to 8.5	<8.0 or >8.5	-	-	-
	Mixed Fe-Cu	C	8.8 to 9.1	<8.8 or >9.1	-	-	-
Water Cation Conductivity (µS/cm)		C	< 0.25	0.25 to 0.45	>0.45 to 0.85	>0.85 to 1.0	> 1.0
Steam Cation Conductivity (µS/cm)		W	< 0.25	0.25 to 0.45	>0.45 to 0.85	>0.85 to 1.0	>1.0
ORP (mV)	All ferrous	T	0 to +100	-	-	-	-
	Mixed Fe-Cu	T	-350 to -300	-	-	-	-
Hydrazine (ppb)	All ferrous	T	0 to 10	> 10	-	-	-
	Mixed Fe-Cu	T	< 20	> 20	-	-	-
Dissolved Oxygen (ppb) (see Notes 5 and 6)	All ferrous	C	< 7	> 7	-	-	-
	All stainless (Water Temp ≤ 50 C)	C	< 800	> 800	-	-	-
	(Water Temp ≤ 100 C)	C	< 300	> 300	-	-	-
	Mixed Fe-Cu	C	< 5	> 5	-	-	-
Sodium (ppb)		W	< 6	6 to 12	>12 to 24	> 24 to 30	> 30
Chloride (Organic and inorganic) (ppb)		T	< 6	6 to 12	>12 to 24	> 24 to 30	> 30
Sulfate (Organic and Inorganic) (ppb)		T	< 6	6 to 12	>12 to 24	> 24 to 30	> 30
Silica (ppb)		D	< 20	20 to 40	>40 to 80	> 80 to 100	> 100
Iron (ppb)		W	< 10	10 – 20	>20 to 40	> 40 to 50	> 50
Copper (ppb)		W	< 2	2 to 4	>4 to 8	> 8 to 10	> 10
Total Organic Carbon (TOC) (ppb)		W	< 100	> 100	-	-	-
Hardness (ppb)		T	< 1	> 1	-	-	-
Suspended Solids (ppb) (see Note 4)		T	Not detectable	-	-	-	-

* Nomenclature and notes follow Table 2. Action levels are given in Section 2.2.

Table 1.0 - All volatile Treatment (AVT) without Reheat

Parameter	Monitoring Frequency	Target Value	Action Level 1	Action Level 2	Action Level 3	Action Level 4
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pH (see Note 7)	All ferrous	C	9.3 to 9.6	<9.3 or > 9.6	-	-	-
	All stainless	C	8.0 to 8.5	<8.0 or >8.5	-	-	-
	Mixed Fe-Cu	C	8.8 to 9.1	<8.8 or >9.1	-	-	-
Water Cation Conductivity (μS/cm)		C	< 0.15	0.15 to 0.25	0.25 to 0.45	>0.45 to 0.5	>0.5
Steam Cation Conductivity (μS/cm)		W	< 0.15	0.15 to 0.25	0.25 to 0.45	>0.45 to 0.5	>0.5
ORP (mV)	All ferrous	T	0 to +100	-	-	-	-
	Mixed Fe-Cu	T	-350 to -300	-	-	-	-
Hydrazine (ppb)	All ferrous	T	0 to 10	> 10	-	-	-
	Mixed Fe-Cu	T	< 20	> 20	-	-	-
Dissolved Oxygen (ppb) (see Notes 5 and 6)	All ferrous	C	< 7	> 7	-	-	-
	All stainless (Water Temp ≤ 50 C)	C	< 800	> 800	-	-	-
	(Water Temp ≤ 100 C)	C	< 300	> 300	-	-	-
	Mixed Fe-Cu	C	< 5	> 5	-	-	-
Sodium (ppb)		W	< 3	3 to 6	6 to 12	> 12 to 15	>15
Chloride (organic and inorganic) (ppb)		T	< 3	3 to 6	6 to 12	> 12 to 15	>15
Sulfate (organic and inorganic) (ppb)		T	< 3	3 to 6	6 to 12	> 12 to 15	>15
Silica (ppb)		D	< 10	10 to 20	20 to 40	> 40 to 50	>50
Iron (ppb)		W	< 10	10 to 20	20 to 40	> 40 to 50	>50
Copper (ppb)		W	< 2	2 to 4	4 to 8	> 8 to 10	>10
Total Organic Carbon (TOC) (ppb)		W	< 100	> 100	-	-	-
Hardness (ppb)		T	< 1	> 1	-	-	-
Suspended Solids (see Note 4)		T	Not detectable	--	-	-	-

* Nomenclature and notes follow Table 2. Action levels are given in Section 2.2.

Table 2.0 - All-volatile Treatment (AVT) with Reheat

Nomenclature:

C = continuous

D = grab sample, once per day

W = grab sample, once per week

T = troubleshooting and commissioning

Notes (Table 1 and Table 2):

- 1) Conductivity and pH measured at 25°C.
- 2) Grab samples are to be more frequent during startup. Grab samples should be once per day until benchmark levels are obtained.
- 3) In start-up situations feedwater must be circulated to reduce the dissolved material and suspended particles and should not be introduced into the OTSG until the cation conductivity is below $1.0 \mu\text{S/cm}$ (or $0.27 \mu\text{S/cm}$ for specific conductivity)
- 4) Suspended solids must be prevented to avoid clogging of feedwater orifices. Suspended solids is commonly measured by examining the undissolved material trapped on a 0.45 micrometer filter after filtration. Material that passes through is referred to as dissolved solids.
- 5) IST can review the allowable oxygen levels for feedwater temperatures less than 50°C.
- 6) IST can review the allowable oxygen levels for systems with feedwater piping fabricated from stabilized stainless steel material (i.e. 347SS, 321SS etc.).
- 7) The recommended pH value for all stainless metallurgy is based on achieving improved condensate polisher performance. The pH values recommended for all ferrous metallurgy (i.e. 9.3 to 9.6) are also acceptable for all stainless metallurgy. The pH values recommended for all ferrous metallurgy (i.e. 9.3 to 9.6) should be used for a system with both ferrous and stainless metallurgy.

2.2 Action Levels

Operation at the lowest achievable impurity levels, with the shortest and least frequent excursions, is the most desirable mode of operation. The probability of corrosion damage and deposit formation grows significantly with increasing impurity concentration, and the damage is proportional to the exposure time. When corrosive impurities concentrate on metal surfaces, the breakdown of passivity (damage to the protective oxide layer) occurs within a few minutes to several hours.

To give more flexibility in the water and steam chemistry control, particularly during startups, three action levels are recommended. The target values for Action Levels 1, 2, and 3 were established to allow for and provide guidance during transient or abnormal operating conditions. If the problem is not corrected within the time allotted to each action level, the next higher action level takes effect.

Normal - Values are consistent with long-term system reliability. A safety margin has been provided to avoid concentration of contaminants at surfaces.

Action Level 1 - There is potential for the accumulation of contaminants and corrosion. Normal Limit can be exceeded for one week with the total yearly accumulation of two weeks. If the time allotted is exceeded an orderly shutdown should occur.

Action Level 2 - The accumulation of impurities and corrosion will occur. Operation is limited to 24 hours with the total yearly accumulation of 48 hours. If the time allotted is exceeded an orderly shutdown should occur.

Action Level 3 - The accumulation of impurities and corrosion will occur very quickly. Operation is limited to 4 hours maximum with the total yearly accumulation of 8 hours. Damage to the OTSG can occur when operating in this condition and immediate action is required to return the feedwater to the target value.

During excursions, when the impurity concentration increases sharply, the accumulation of impurities in the cycle occurs quickly, but the subsequent cleanup upon return to good chemistry may take weeks. Therefore, yearly time accumulations were also established as a guide. If the unit is shutdown due to water or steam chemistry (i.e. a major condenser leak), it should be an orderly shutdown, not a trip.

Action Level 4 - Impurity levels are too high and severe damage may occur to the OTSG. Immediate orderly shutdown of the OTSG is recommended.

2.3 Corrective Actions

Typical corrective actions to respond to out-of-specification steam and/or water chemistry conditions are listed in this Section. These corrective actions are not meant to be all-inclusive or universally applicable. Each utility and/or plant should establish plant-specific corrective actions that consider plant design features and other plant-specific concerns. Successful implementation of this specification requires proper training of operators and is the responsibility of the owner. **ONLY AFTER DETERMINING THE ROOT CAUSES OF AN EXCURSION CAN A PERMANENT SOLUTION BE SELECTED.**

The action to be taken to confirm and correct water and the time to confirm and correct a water chemistry upset depends on the severity of the chemical excursion. On-line and grab sample analysis data must be used to determine the source(s) of ingress of various impurities. Possible causes of feedwater chemistry excursions are described below. Corrective actions for each monitored parameter are listed below

Jumper Tube Installation Proposal

Date: November 27, 2013

Customer Reference: Glenarm Repowering – Jumper tube installation

IST Reference: P12079-00 Jumper Tubes

To the BOP contractor bidding the construction of the Glenarm Repowering Project:

The following estimate is based on working a 6 x 10-hr/dy workweek Monday through Saturday, with Sunday as a scheduled off-day. Two (2) travel days (one in & one out) have also been included for all three (3) IST personnel. If additional weekend work or overtime is required, additional charges will be invoiced per the IST standard rate sheet, based on the approved signed time sheets from site. No stat-holiday period work time has been accounted for in this quotation. Any unforeseeable circumstances beyond our control causing delays will be charged based on the standard rate sheet, in accordance with the signed timesheets.

No allowance has been given for time on site for hydrostatic testing after the jumper tube welding is completed, as the external pipe welding to each unit cannot commence until after the tube welding is completed. Therefore it is presumed that this testing will be performed at a later date. IST representation for the witness of the final Sect-1 hydrostatic test that includes the boiler external piping is presumed to be performed at a later visit (which is not included in this pricing). Test plugs for steam and feedwater headers can be made available for shipment with the tools, and a pneumatic test can be performed on the site jumper welds prior to IST personnel's departure from site.

IST field service scope included in this proposal:

- Removal and reinstatement (if required) of any restraint assemblies, end-seal floors, or other OTSG components necessary to provide access to the press-part working area.
- Installation and welding of (41) jumper tube assemblies per OTSG Unit, totaling 123 x 1.25"-diameter welds, and 41 x ½"-diameter welds per boiler. All tube welding will be performed using an automatic 'tig' orbital welding process.
- Installation of 41-each per boiler, packing-gland seal bushings at the lower SCR catalyst rear floor jumper-tube penetrations.
- Engineering and administration time for the implementation of the above scope.
- All IST personnel travel & labour time, air & ground transportation costs, and subsistence for two weeks.
- Packing and shipment (return) of tools and equipment to implement the installation.
- Consumables, excluding argon gas.
- Preparation of job Quality Package including ASME Section I Data Report Forms, for submission and review by the local Authorized Inspector in the jurisdiction.

IST personnel will come prepared with all the tools necessary to execute the internal jumper tube pressure-part work, but will require some logistical support from the customer and their contractor personnel during the execution. To clarify responsibilities required by the customer / contractor for support provisions, please note the following:

Customer's Scope:

In order to accomplish the necessary tasks it will be necessary for the customer to provide the following:

1. Provision of electric power for IST portable transformers requiring 480V, 30 Amp service to support operation of orbital welding units and electric tools.
2. Electrician for initial hook up and disconnect. (3 hrs total est'd)
3. Provision of compressed air for use of hand operated pneumatic milling tools.
4. Provision of argon gas; estimated requirement is (1) x 12 bottle - manifold pack, plus four (4) individual loose bottles of 2300 psi argon per boiler.
5. Availability of a propane tank (if req'd), in the event feedwater header lines require to be tag torched dry, if evidence of moisture is apparent.
6. Site safety induction of IST personnel.
7. Designated dry laydown area for IST tool crate in close proximity to the OTSG's (preferably beneath the inlet plenum).
8. Disposal container for miscellaneous refuse (if req'd).
9. Provision of air quality testing for confined space prior to access into unit.
10. Provision of safety door watch personnel throughout the work period.
11. Provision of (2) x supplemental workers (boilermaker or similar trades designation) for support setting-up equipment and providing mechanical/trades support throughout the job as the need dictates.
12. Access to lunchroom and toilette facilities for on-site personnel.
13. Provision of off-loading capabilities for equipment arriving at site.
14. Provision of scaffolding/platforms as required for access to all internal working area levels where orbital welding is to be completed.
15. Provision of external scaffolding access at feedwater inlet box if platform access is not in place. This is required to access the HP feedwater inlet header and flex tubes.
16. All rear internal joint kits in the proximity of the jumper tube installation must be in place prior to the welding technicians arrival on site.
17. Provision of on-site permits and safe lock-out of any relevant equipment.

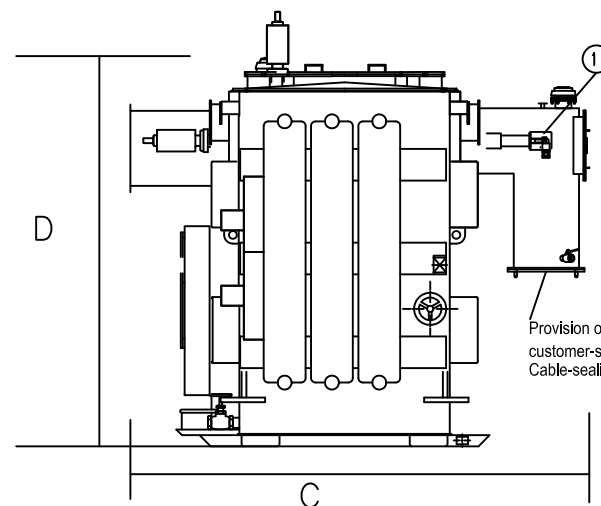
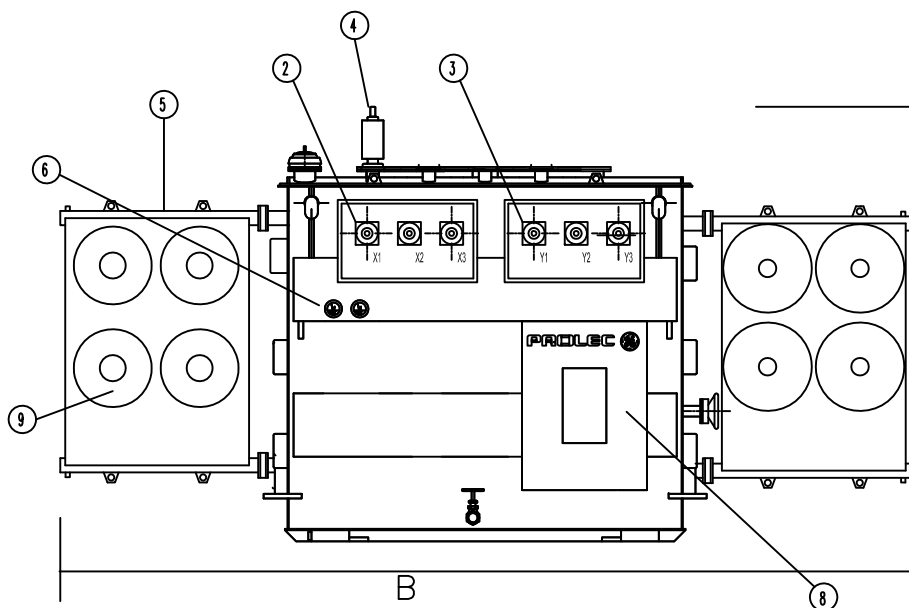
For hydrostatic testing activities at a later point in time, and not included in this price, following the completion of jumper-tube welding and boiler external piping, the customer / contractor will be responsible for the following:

- a) Supply of ample demineralized water and pressurizing equipment to perform a hydrostatic test of the steam generator(s) once installation is complete.
- b) Any temporary boiler internal propane heating (if req'd-seasonal), to raise feedwater and tubing temperature to the acceptable code level of 21°C.
- c) Coordination with and contracting of local AI in the jurisdiction.

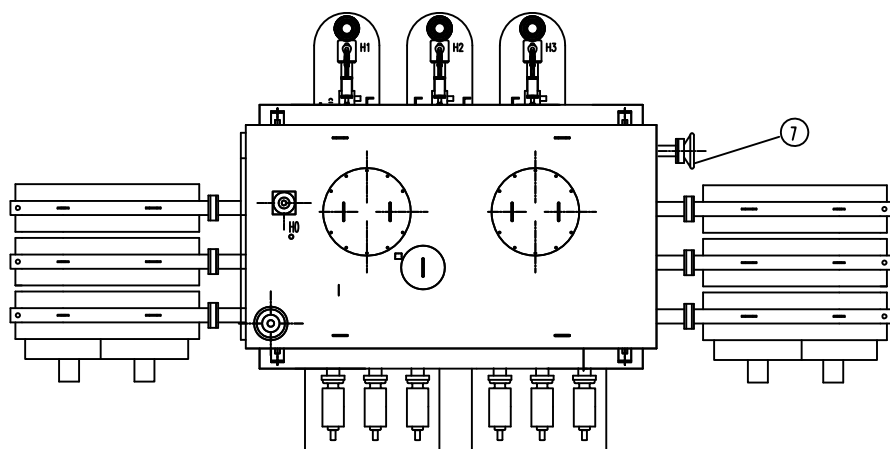
Estimated cost for the above work is \$75,000 CAD

Best Regards,

Richard Welk,
Field Service Technical Advisor



Provision only for installing
customer-supplied cable sealing ends
Cable-sealings ends (slip-on terminators) by customer



- 1.- H. V. BUSHINGS "H"
- 2.- L. V. BUSHINGS "X"
- 3.- L. V. BUSHINGS "Y"
- 4.- NEUTRAL BUSHING
- 5.- RADIATORS
- 6.- INSTRUMENTS
- 7.- NO LOAD TAP CHANGER
- 8.- CONTROL CABINET
- 9.- FANS (IF SUPPLY)

NOTE: THIS DRAWING IS A PRELIMINARY PROPOSAL AND DOES NOT INDICATE THE EXACT DETAILS OF CONSTRUCTION, ARRANGEMENT OF ACCESSORIES OR THE FINAL DIMENSIONS OF THE TRANSFORMER. THIS INFORMATION SHOULD NOT BE USED FOR FINAL CONSTRUCTION ARRANGEMENTS OR FOR THE FOUNDATION UNLESS SPECIFICALLY APPROVED BY THE FACTORY. ALL DIMENSIONS AND WEIGHTS ARE APPROXIMATE

TECHNICAL PROPOSAL INFORMATION

Customer: GE AERO Date: 08/20/13
 Proposal No: 131-03751 Spec No: SECTION 261200 Item No: 2217321/D

RATING						
Type	Transformer	Class	H Winding	X Winding	Y Winding	
Phase	3		34.5 Wye kV	13.8 Delta kV	13.8 Delta kV	
Hertz	60	KNAN	57,000 KVA	45,000 KVA	12,000 KVA	
Temp Rise	65 °C	KNAF	76,000 KVA	60,000 KVA	16,000 KVA	
Insul Liquid	FR-3	KNAF	95,000 KVA	75,000 KVA	20,000 KVA	
		-	- KVA	- KVA	- KVA	

ADDITIONAL TAP VOLTAGES						
H Winding (Kv)	-	DETC				
X Winding (Kv)	-	-				
Y Winding (Kv)	-					
CONNECTIONS FOR OPERATION						
Transformers in Bank	To Transformer From	Phase	Connected	To Transformer To	Phase	Connected
-	-	-	-	-	-	-

PERFORMANCE BASED ON A LOADING OF				DIELECTRIC TESTS		INSULATION LEVELS		
						ITEMS	Basic Lightning Impulse (kV)	
							Winding	Bushing
H Winding	34.5 kV	57.0 MVA		Applied Voltage (To other winding and ground)	H Winding 50 kV	H Line	200	200
X Winding	13.8 kV	45.0 MVA			X Winding 34 kV	H neutral	150	150
Y Winding	13.8 kV	12.0 MVA			Y Winding 34 kV	X line	110	110
-	-	-	-	Induced Voltage	7200 cycles 69 kV	Y line	110	110
-	-	-	-		- kV	-	-	-

PERFORMANCE DATA, Based on 85 °C Reference Temperature, 57 MVA Altitude: 1000 Mts.					
Losses and Exciting Current				Regulation Approximate	
Excitation	% Ex	No Load Kw (20°C)	Total Loss Kw	Power Factor	% Regulation
100%	0.355	36	253	0.80	8.387
110%	0.512	47 *	264 *	1.0	1.181
-	-	* Not Guaranteed		-	-

AUXILIARY (COOLING) LOSSES			
Transformer KVA	Class	KWatts Loss	
57,000	-	KNAN	0.0
76,000	-	KNAF	2.5
95,000	-	KNAF	5.0
-	-	-	-
-	-	-	-
Average Sound Level 76/78/79 dB ONAN/ONAF/ONAF			

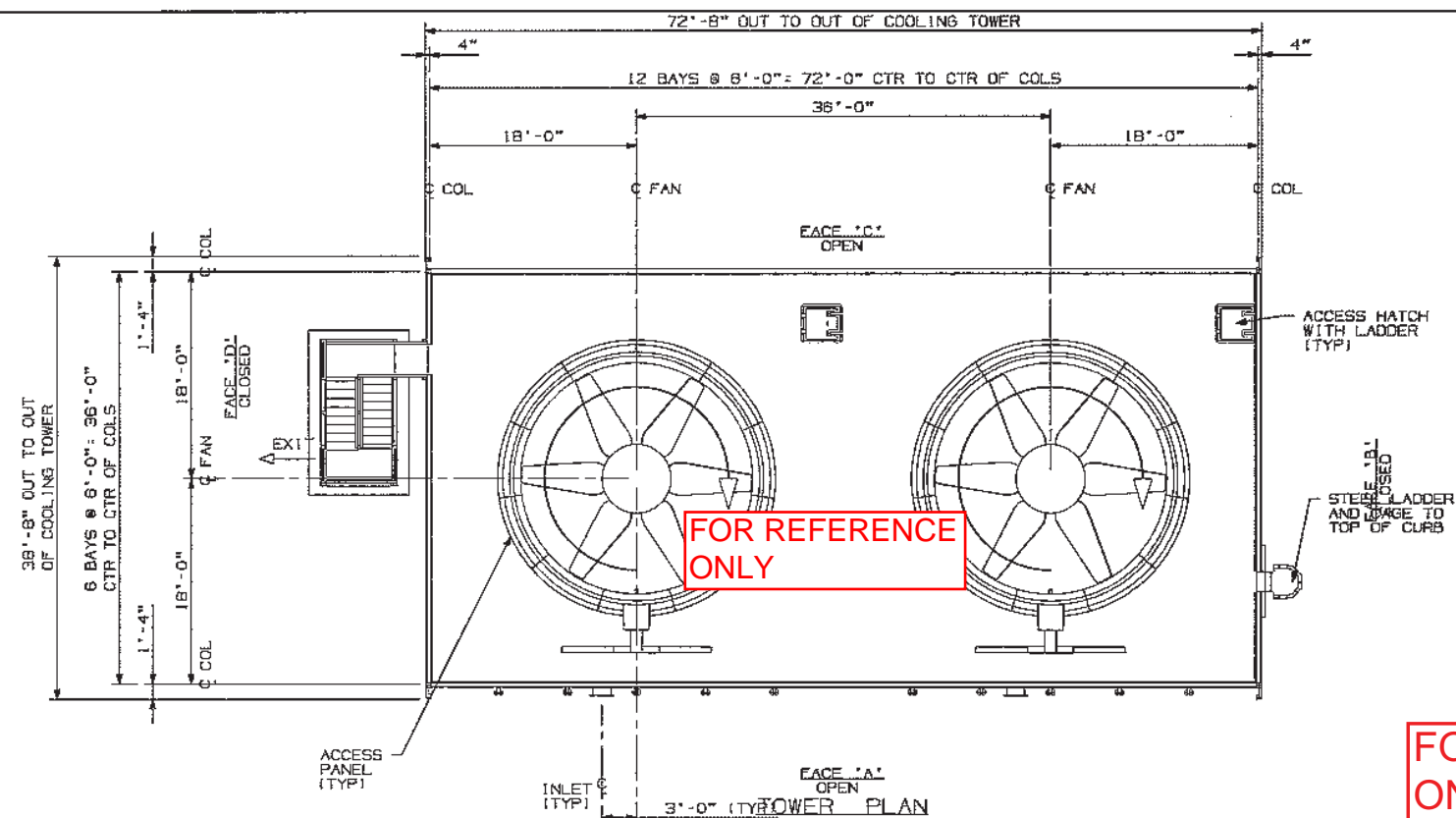
PERCENT IMPEDANCE VOLTS					
% IZ	Between Windings	At kVA	% IZ Zero	Between Windings	At kVA
12.66	H-X	57,000	-	-	-
47.5*	H-Y	57,000	-	-	-
35.1*	X-Y	57,000	-	-	-

* APPROXIMATE ONLY, NOT GUARANTEED

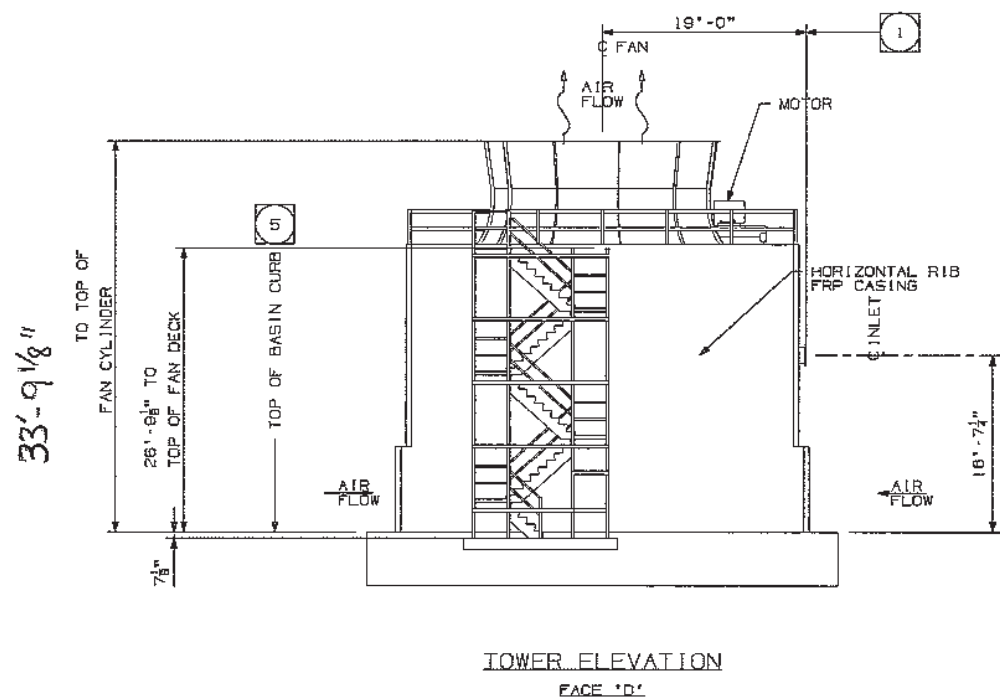
EFFICIENCIES (p.f=1) AT 57 MVA				
Load	Full Load	3/4 Load	1/2 Load	1/4 Load
%	99.558	99.632	99.684	99.653

MECHANICAL DATA	
Not for Construction Purposes	
Outline Dwg No:	221732D1
Dimensions (Approximate)	Ft. (Mts.)
Height (A)	17.5 (5.32)
Width (B)	31.7 (9.65)
Depth (C)	16.5 (5.02)
Height over Cover (D)	14.0 (4.27)
Untanking (Plus slings) (E)	25.0 (7.61)
Shipping Dimensions:Ft WxDxH	21.6 x 12.0 x 14.1
Masses (Approximate)	pounds (Kg)
Core and Coils	143,360 (65,030)
Tank and Fittings	63,210 (28,680)
Liquid 11,580 Gal	89,180 (40,450)
Total Mass	295,750 (134,160)
Shipping without OIL	189,840 (86,110)
Shipping with OIL	-

3D CAD MASTER PART NAME:



FOR REFERENCE ONLY



GENERAL NOTES

1. INLET INFORMATION: SPX CT PIPING STOPS AT THE FACE OF A 18 in. DIAMETER, 25 PSI. FLAT-FACED RTR FLANGE WHICH IS 15/16 in. (1 1/2 in. - 1/8 in.) THICK. THERE ARE 16 - 1 1/4 in. DIAMETER BOLT HOLES ON A 22 3/4 in. DIAMETER BOLT CIRCLE. BOLT HOLES STRADDLE THE PIPE CENTERLINES. PURCHASER IS TO FURNISH ALL CONNECTING HARDWARE (INCLUDING STANDARD CUT WASHERS FOR THE RTR FLANGE. FLANGE DRILLING CONFORMS TO CLASS 150 ASME B16.5 SPECIFICATIONS. THE FLANGE GASKET IS 3/8 in. THICK FULL-FACE SOFT NEOPRENE OF SHORE DUROMETER 50 +/-5 (FURNISHED BY SPX CT).

2. CAUTION: SPX CT PIPE SUPPORTS ARE DESIGNED TO SUPPORT ONLY THE WEIGHT OF THE PIPE AND WATER WITHIN THE LIMITS OF THE INLET FLANGE. CARE MUST BE TAKEN WHEN INSTALLING THE CONNECTING PIPING TO AVOID OVERLOADING OR DAMAGING THE TOWER STRUCTURE.

3. INSTALLER NOTE: CONNECTING PIPING MUST BE PROPERLY ALIGNED AT INSTALLATION TO AVOID DAMAGING OR MOVING THE RTR PIPE WHEN TIGHTENING THE FLANGE BOLTS.

4. BYPASS SYSTEM: REDUCED WATER FLOW OVER A COOLING TOWER IN COLD CLIMATES CAN RESULT IN ICE FORMATION IN THE FILL. IF THE PURCHASER'S APPLICATION REQUIRES A BYPASS SYSTEM, ITS DESIGN MUST BE REVIEWED BY SPX CT ENGINEERING.

5. CURB REFERENCE: TOP OF BASIN CURB REFERENCE IS TO BE THE HIGHEST POINT OF THE BASIN CURB WALL. FAILURE TO NOTE THIS COULD RESULT IN A MISALIGNMENT OF THE RISER TO INLET CONNECTIONS! AN INCORRECT STAIRPAD ELEVATION, AND A DECREASE IN THE AIR INLET ELEVATION THUS DECREASING COOLING TOWER PERFORMANCE.

REFER TO GENERAL NOTE

FAN DIAMETER	216
# FAN BLADES	9
MOTOR SIZE	100 HP
INLET DIAMETER	18"
AIR INLET ELEV	8.0'

Preliminary
Drawing

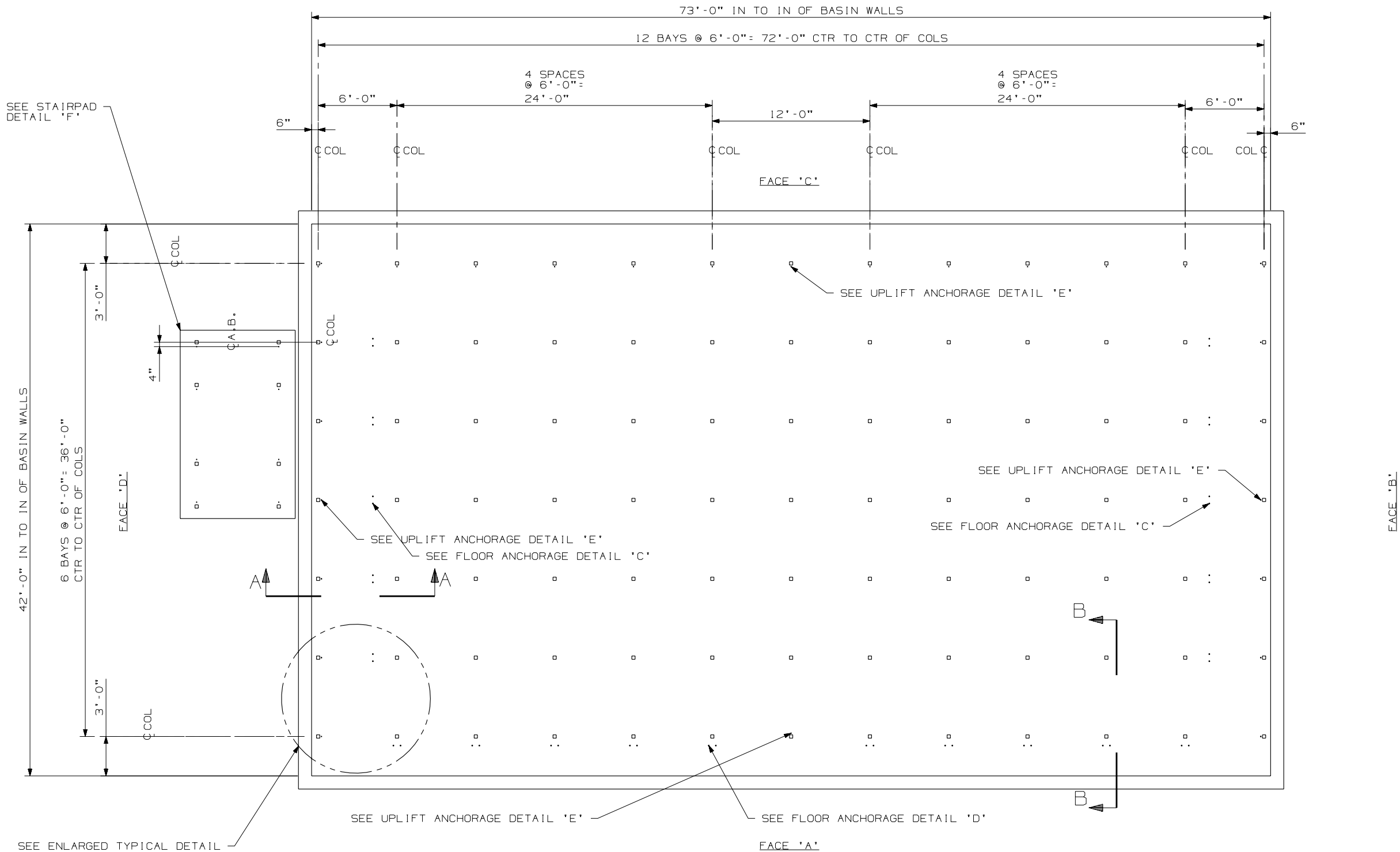
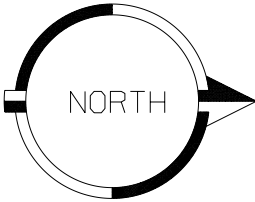
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GE - Glenarm Repowering
LOS ANGELES, CA, United States

E30 NUMBER		SCHEMATIC VIEWS				SPX	
REV. BY		F436A36A5.302A COUNTERFLOW TOWER				COOLING TECHNOLOGIES	
REV. DATE		DESIGN BY	DATE	CHECKED	APPROVED	CHALK NUMBER	PLATE
		QTC	10/22/12			154213807	I-160
						ISSUING NUMBER	SOL.
						JW4838445	-



BASIN PLAN VIEW

*Preliminary
Drawing*

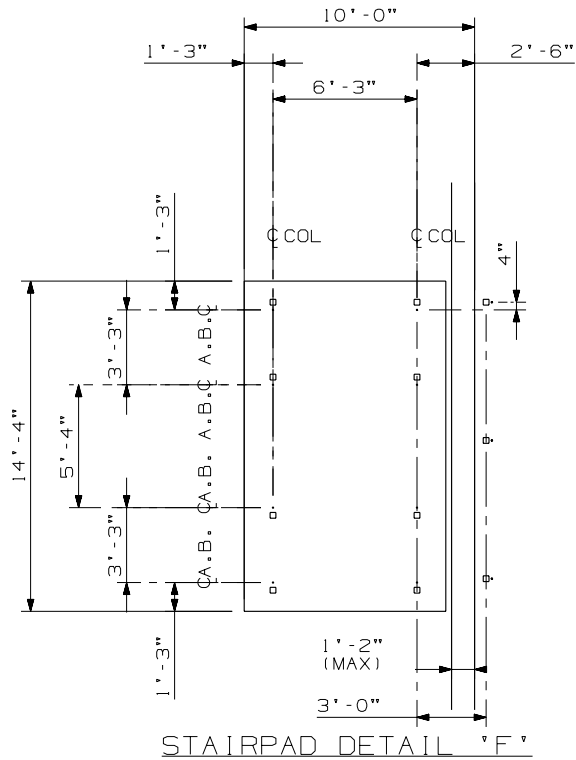
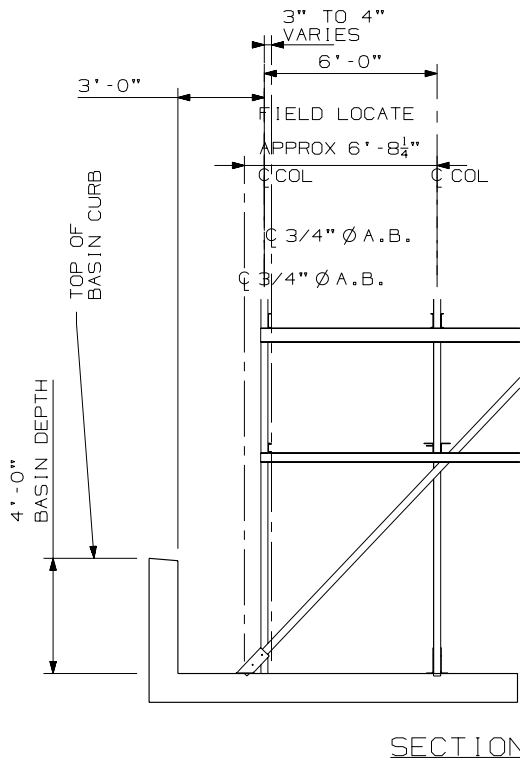
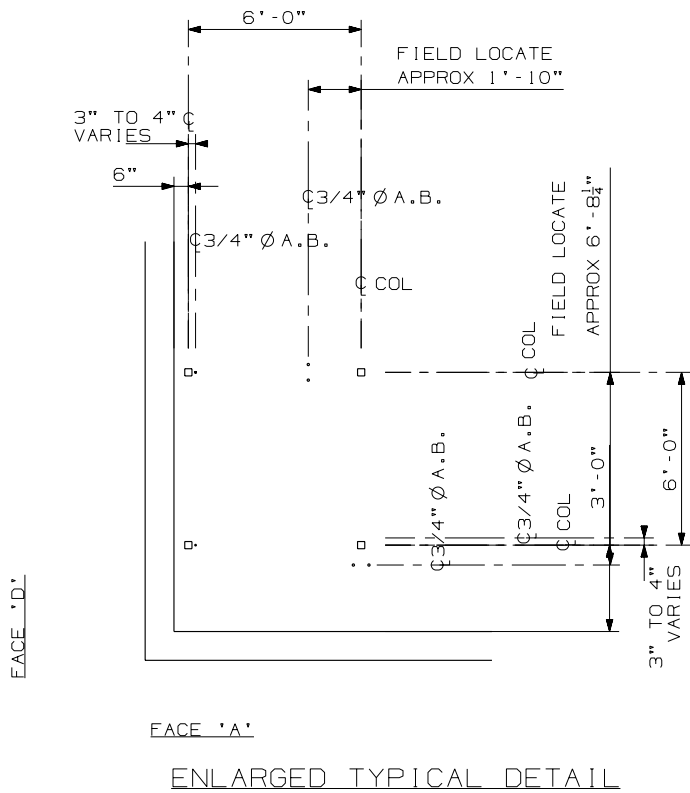
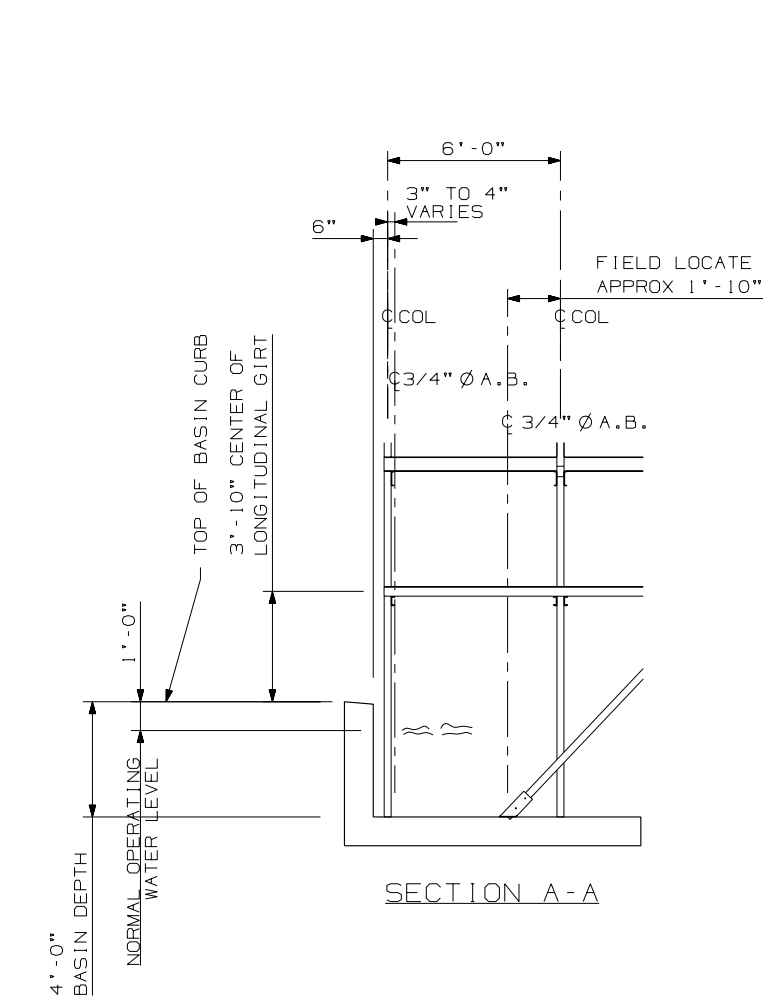
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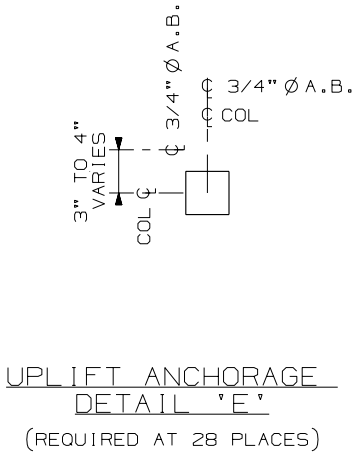
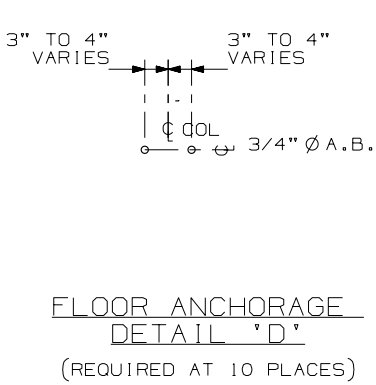
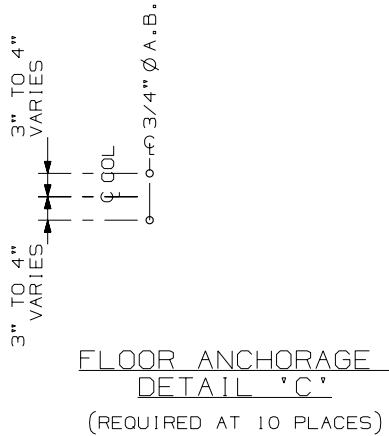
FOR BASIN SECTIONS, DETAILS AND GENERAL NOTES SEE DRAWING JV468844D

ECO NUMBER				BASIN PLAN VIEW F436A36A5.302A COUNTERFLOW TOWER				SPX COOLING TECHNOLOGIES			
REV. BY	CHECKED			DATE	CHECKED	APPROVED	ORDER NUMBER	PLOT	DRAWING NUMBER	REV.	
		DRAWN BY		10/22/12			154213807	I=101	JV468844B	-	
		OTC									



STAIRPAD NOTES

REFER TO BASIN PLAN FOR STAIRPAD ORIENTATION.
TOP OF STAIRPAD TO BE 7 1/8 BELOW TOP OF BASIN CURB.
MAXIMUM DEAD LOAD ON ANY STAIR COLUMN IS 1250 POUNDS.



GENERAL NOTES

1. BASIN CONSTRUCTION: PURCHASER TO DESIGN, CONSTRUCT, AND FURNISH THE COOLING TOWER FOUNDATION TO SUIT THE DIMENSIONS OF THESE DRAWINGS. THE BASIN DESIGNER SHOULD REFER TO THE SCHEMATIC DRAWING AND AVOID LOCATION OF SUMP SCREENS, PUMPS AND ADJACENT EQUIPMENT THAT WILL INTERFERE WITH THE STAIRWAY, LADDER, OR OTHER TOWER EQUIPMENT.
2. PURCHASER TO DESIGN, LOCATE, AND FURNISH THE SUMP TO SUIT THE JOB REQUIREMENTS.
3. CONCRETE FINISH: CONCRETE SURFACES AT THE TOWER ANCHORAGE POINTS MUST BE TROWELLED TO A SMOOTH FINISH BY PURCHASER. THIS WORK MUST BE COMPLETED BEFORE TOWER CONSTRUCTION BEGINS. TOWER COLUMNS ARE FIELD CUT TO FIT THE BASIN FLOOR A MAXIMUM OF 4'-0 INCH BELOW THE TOP OF THE BASIN CURB.
4. BASIN FLOOR TO BE FLAT.
5. ANCHOR BOLTS: TOWER AND STAIR ANCHOR BOLTS ARE 3/4 INCH DIAMETER (76 REQUIRED) ALL THREAD WITH 6 5/8 INCHES MINIMUM EMBEDMENT AND 2 INCHES MINIMUM PROJECTION 1/8 INCH ABOVE THE FINISHED CONCRETE.
6. UPLIFT ANCHORAGE ON PERIMETER TOWER COLUMNS CAN BE INSTALLED ON ANY FACE OF THE COLUMN PROVIDED IT DOES NOT INTERFERE WITH THE DIAGONAL ANCHORAGE AND IS LOCATED WITH THE ANCHOR BOLT A MINIMUM OF 6 INCHES FROM ANY CONCRETE EDGE.
7. SPX CT TO FURNISH AND INSTALL ALL ADHESIVE ANCHORS COMPLETE WITH NUT AND WASHER AT TIME OF TOWER ERECTION.
8. FOR ANCHOR BOLT DESIGN, THE MINIMUM 28-DAY CONCRETE COMPRESSIVE STRENGTH IS TO BE 4,000 PSI. DESIGN IS BASED ON UNCRACKED CONCRETE.
9. CURB REFERENCE: TOP OF BASIN CURB REFERENCE IS TO BE THE HIGHEST POINT OF THE BASIN CURB WALL. FAILURE TO NOTE THIS COULD RESULT IN A MISALIGNMENT OF THE RISER TO INLET CONNECTION(S), AN INCORRECT STAIRPAD ELEVATION, AND A DECREASE IN THE AIR INLET ELEVATION THUS DECREASING COOLING TOWER PERFORMANCE.
10. DIFFERENTIAL SETTLEMENT CRITERIA: THE MAXIMUM SETTLEMENT THAT THE COOLING TOWER CAN ABSORB IS 1/8 INCH IN 6 FEET-0 INCHES, UP TO 1/2 INCH MAXIMUM IN TOWER WIDTH AND 1 INCH MAXIMUM IN TOWER LENGTH.
11. BASIN DESIGNER REBAR NOTE: LOCATE REINFORCING STEEL TO PREVENT INTERFERENCE WITH ANCHOR BOLTS. ANCHOR BOLT DIMENSIONS ARE LISTED AS APPROXIMATE TO ACCOUNT FOR MINOR IMPERFECTIONS IN BASIN LEVELNESS. LOCATE REINFORCING STEEL TO ALLOW 3 INCHES MINIMUM CLEARANCE TO ANCHOR BOLTS.

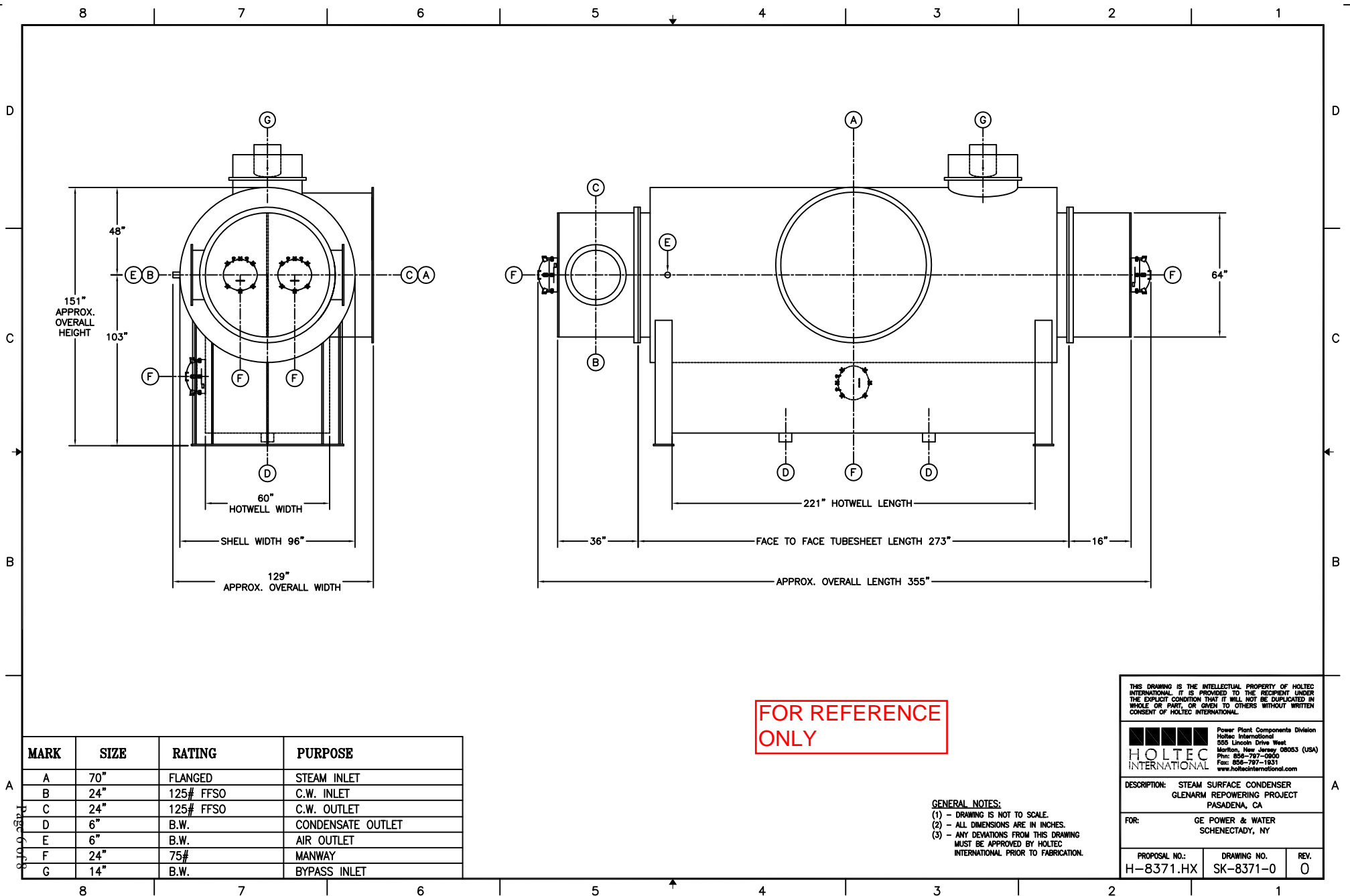
Preliminary
Drawing

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consideration and discussion.

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ECO NUMBER		BASIN SECTIONS & DETAILS				GE - Glenarm Repowering LOS ANGELES, CA, United States			
REV. BY		CHECKED		F436A36A5.302A COUNTERFLOW TOWER		SPX COOLING TECHNOLOGIES			
REV. DATE		DRAWN BY		DATE		CHECKED		APPROVED	
		OTC		10/22/12					
ORDER NUMBER		DRAWING NUMBER		PLOT		REV.			
154213807		JV4688440		VARIES		-			

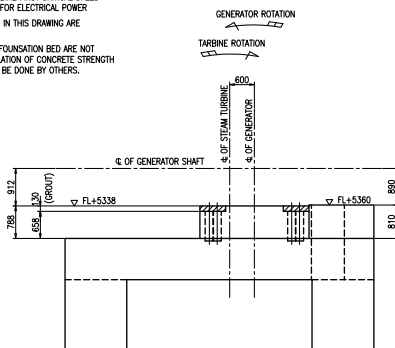


NOTE

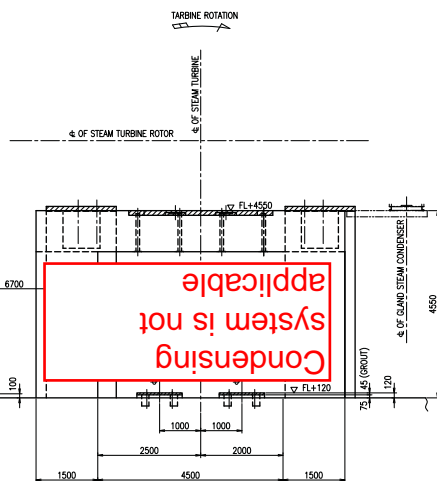
1. REGARDING THE DETAIL OF LOADING DATA. REFER TO THE ANOTHER DRAWING.
2. THE DISTANCE BETWEEN ALL SLEEVES OF FOUNDATION SHOULD BE KEPT WITH IN A TOLERANCE OF ± 3 mm
3. SHOWS PRE-NON-SHRINK GROUT FOR L
4. SHOWS FINAL NON-SHRINK GROUT AFTER
5. THE NATURAL FREQUENCY OF T/G BED SHALL BE NOT MATCH WITH FOLLOWINGS.
103.3Hz FOR TURBINE SPEED
25Hz FOR GENERATOR SPEED
50.9Hz FOR TURBINE FIRST CRITICAL SPEED
50Hz & 100Hz FOR ELECTRICAL POWER
SUPPLIED BY CUSTOMER
6. EMBEDDED PARTS AS SHOWN IN THIS DRAWING ARE SUPPLIED BY CUSTOMER
7. THE OUTLINE DIMENSION OF FOUNDATION BED ARE NOT DETERMINED BY THE CALCULATION OF CONCRETE STRENGTH SO. THE CALCULATION MUST BE DONE BY OTHERS.

FOR REFERENCE

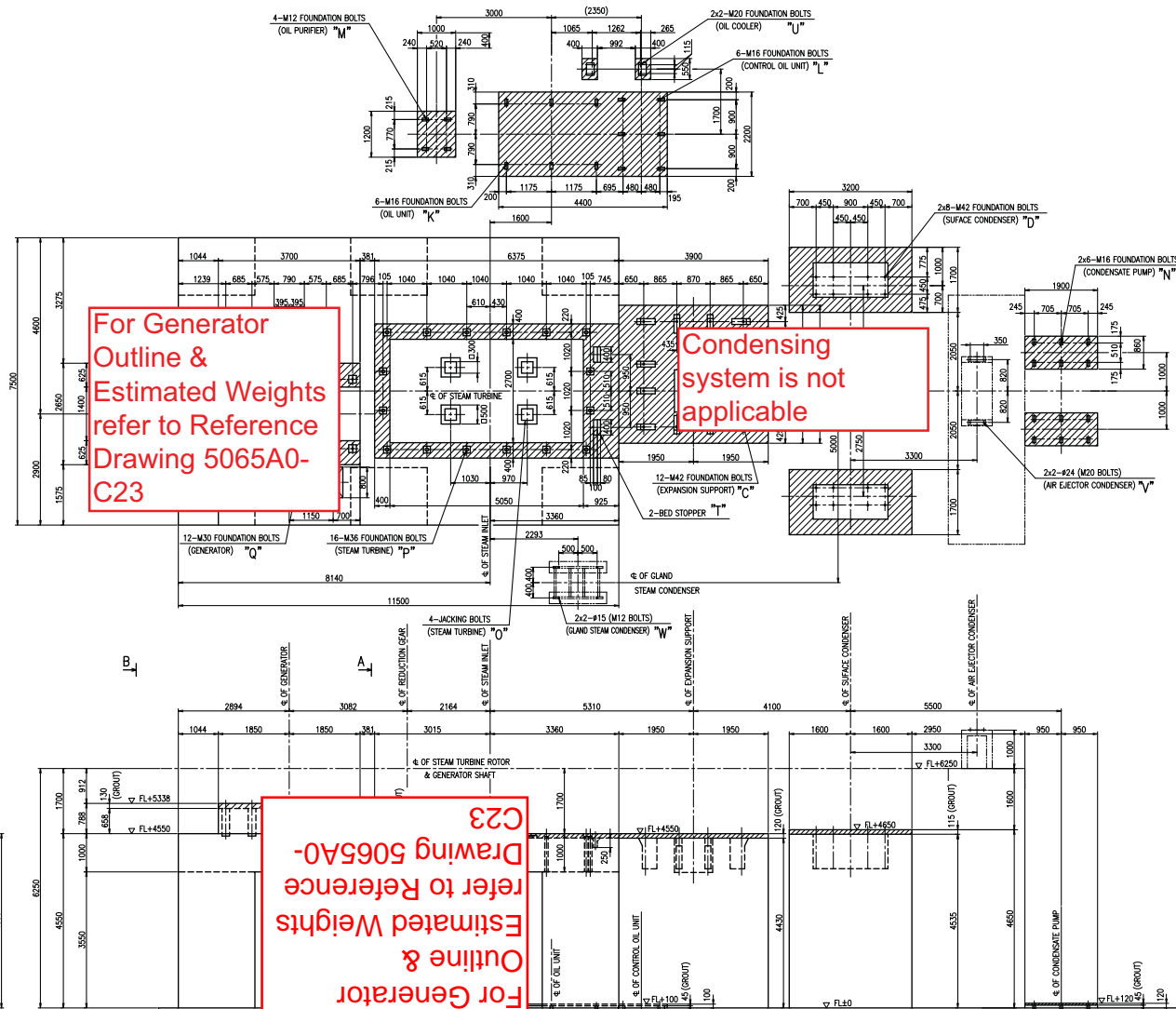
TYPICAL, FOR
REFERENCE ONLY.



VIEW B - B



SECTION A - A



For Generator
Outline &
Estimated Weights
refer to Reference
Drawing 5065A0-
C23

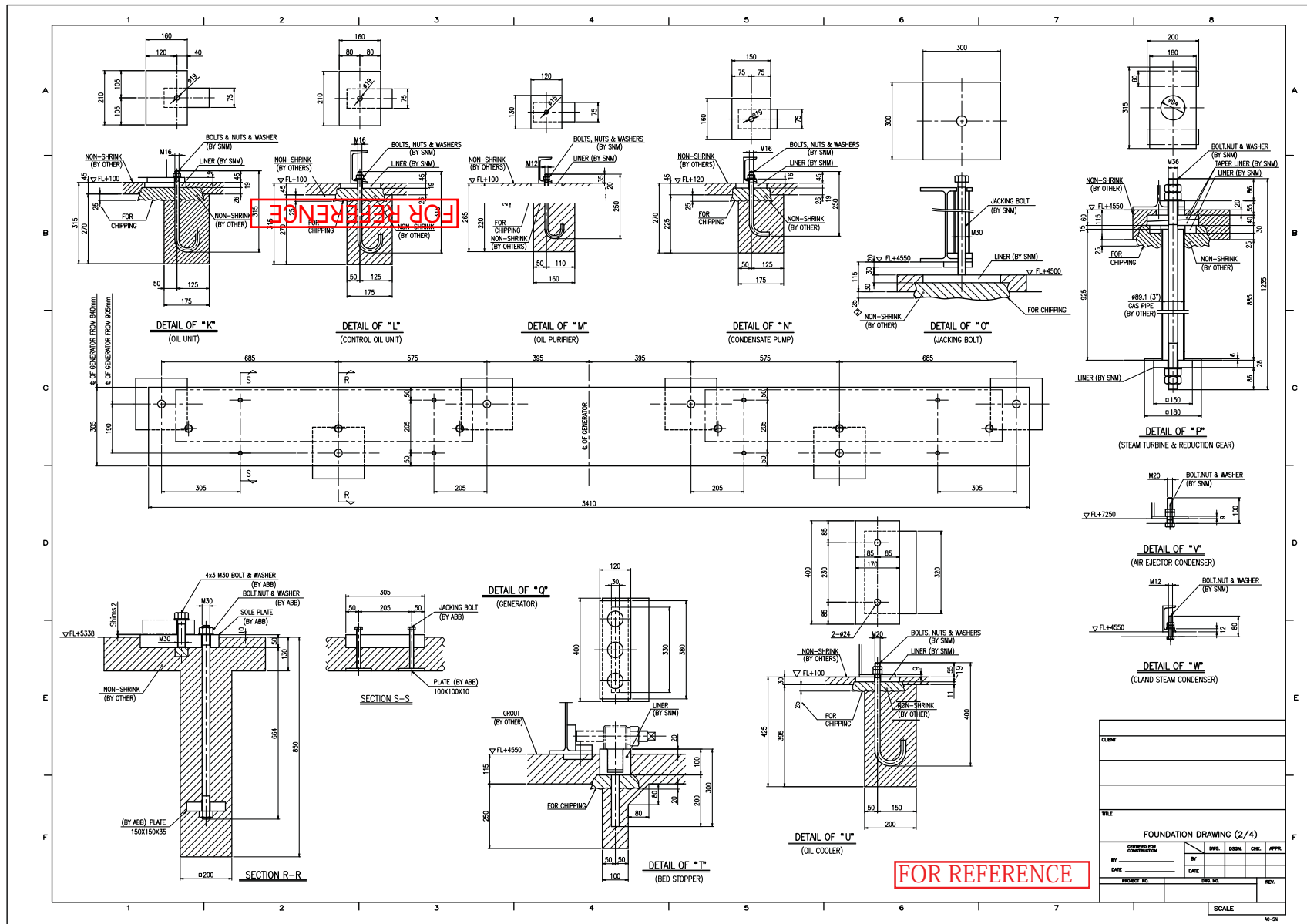
Condensing
system is not
applicable

For Generator
Outline &
Estimated Weights
refer to Reference
Drawing 5065A0-
C23

TYPICAL, FOR
REFERENCE ONLY.

FOR REFERENCE

TITLE				
FOUNDATION DRAWING (1/4)				
BY	DWG.	DSGN.	CHK.	APPR.
DATE	DATE			
PROJECT NO.	DWG. NO.			REV.
SCALE				



FOR REFERENCE

TYPICAL, FOR
REFERENCE ONLY.

The Foundation height is depended
on condensing system
arrangement, the minimum height
for the STG is 1,500mm.

CONDENSING SYSTEM IS NOT
APPLICABLE

CONDENSING SYSTEM IS NOT
APPLICABLE

For Generator
Outline &
Estimated Weights
refer to Reference
Drawing 5065A0-
C23

For Generator
Outline &
Estimated Weights
refer to Reference
Drawing 5065A0-
C23

CONDENSING SYSTEM IS NOT
APPLICABLE

CONDENSING SYSTEM IS NOT
APPLICABLE

The Foundation height is depended
on condensing system
arrangement, the minimum height
for the STG is 1,500mm.

LAY OUT											
CERTIFIED FOR CONSTRUCTION											
BY _____		BY _____		DWG.		DSGN.		CHK.		APPR.	
DATE _____		DATE _____									
PROJECT NO.					DWG. NO.					REV.	
PTTUT: 246/50					PTTUT: 33904-PL-004-6						
CTCIT: 07EPC7457					EGAT: 1C3P-3904-PL-M004-06						
					SNM: 11415-0002-10					6	
					SCALE					1 : 60	
										AC-SN	

Loading Data [kN]

Name	Position	Static Load	Dynamic Load(+/-)*			Vacuum Load		
			Vertical	Horizontal	Axial	Axial		
Steam turbine and Reduction gear with base plate	A1	15.86	23.79	3.97	1.59	+/- 16.12		
	A2	15.86	23.79	3.97	1.59	+/- 16.12		
	A3	43.70	65.55	10.93	4.37	+/- 16.12		
	A4	43.70	65.55	10.93	4.37	+/- 16.12		
	A5	31.85	47.78	7.96	3.19	+/- 16.12		
	A6	31.85	47.78	7.96	3.19	+/- 16.12		
	A7	31.85	47.78	7.96	3.19	+/- 16.12		
	A8	31.85	47.78	7.96	3.19	+/- 16.12		
	A9	31.85	47.78	7.96	3.19	+/- 16.12		
	A10	31.85	47.78	7.96	3.19	+/- 16.12		
	A11	43.70	65.55	10.93	4.37	+/- 16.12		
	A12	43.70	65.55	10.93	4.37	+/- 16.12		
	A13	15.86	23.79	3.97	1.59	+/- 16.12		
	A14	15.86	23.79	3.97	1.59	+/- 16.12		
	A15	15.86	23.79	3.97	1.59	+/- 16.12		
	A16	15.86	23.79	3.97	1.59	+/- 16.12		
Generator	B1	28.60	AT RATED TORQUE	-	28.60	N/A	Short Circuit Load (+/-)	-
	B2	28.60		12.20	40.80	N/A		101
	B3	28.60		12.20	40.80	N/A		101
	B4	28.60		12.20	40.80	N/A		101
	B5	28.60		12.20	40.80	N/A		101
	B6	28.60		-	28.60	N/A		-
	B7	28.60		-	28.60	N/A		-
	B8	28.60		-12.20	16.40	N/A		101
	B9	28.60		-12.20	16.40	N/A		101
	B10	28.60		-12.20	16.40	N/A		101
	B11	28.60		-12.20	16.40	N/A		101
	B12	28.60		-	28.60	N/A		-
Connection piece	C1	17.58	17.58	0.74	1.07	N/A		
	C2	17.58	17.58	0.74	1.07	N/A		
	C3	17.58	17.58	0.74	1.07	N/A		
	C4	17.58	17.58	0.74	1.07	N/A		
	C5	17.58	17.58	0.74	1.07	N/A		
	C6	17.58	17.58	0.74	1.07	N/A		
	C7	17.58	17.58	0.74	1.07	N/A		
	C8	17.58	17.58	0.74	1.07	N/A		
	C9	17.58	17.58	0.74	1.07	N/A		
	C10	17.58	17.58	0.74	1.07	N/A		
	C11	17.58	17.58	0.74	1.07	N/A		
	C12	17.58	17.58	0.74	1.07	N/A		
Surface Condenser	D1	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D2	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D3	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D4	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D5	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D6	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D7	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D8	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D9	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D10	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D11	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D12	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D13	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D14	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D15	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	
	D16	31.88	Full (app.)	67.43	N/A	N/A	-/+ 16.12	

Loading Data [kN]

Name	Position	Static Load	Dynamic Load(+/-)*			Vacuum Load
			Vertical	Horizontal	Axial	Axial
Oil unit	E1	Dry (app.) 8. 01	Working (app.) 12. 67	N/A	N/A	N/A
	E2	Dry (app.) 8. 01	Working (app.) 12. 67	N/A	N/A	N/A
	E3	Dry (app.) 8. 01	Working (app.) 12. 67	N/A	N/A	N/A
	E4	Dry (app.) 8. 01	Working (app.) 12. 67	N/A	N/A	N/A
	E5	Dry (app.) 8. 01	Working (app.) 12. 67	N/A	N/A	N/A
	E6	Dry (app.) 8. 01	Working (app.) 12. 67	N/A	N/A	N/A
Control oil pump unit	F1	Dry (app.) 1. 15	Working (app.) 1. 23	N/A	N/A	N/A
	F2	Dry (app.) 1. 15	Working (app.) 1. 23	N/A	N/A	N/A
	F3	Dry (app.) 1. 15	Working (app.) 1. 23	N/A	N/A	N/A
	F4	Dry (app.) 1. 15	Working (app.) 1. 23	N/A	N/A	N/A
	F5	Dry (app.) 1. 15	Working (app.) 1. 23	N/A	N/A	N/A
	F6	Dry (app.) 1. 15	Working (app.) 1. 23	N/A	N/A	N/A
Oil purifier	G1	Dry (app.) 0. 99	Working (app.) 1. 28	N/A	N/A	N/A
	G2	Dry (app.) 0. 99	Working (app.) 1. 28	N/A	N/A	N/A
	G3	Dry (app.) 0. 99	Working (app.) 1. 28	N/A	N/A	N/A
	G4	Dry (app.) 0. 99	Working (app.) 1. 28	N/A	N/A	N/A
Condensate Pump	H1	1. 38	2. 07	0. 35	0. 14	N/A
	H2	1. 38	2. 07	0. 35	0. 14	N/A
	H3	1. 38	2. 07	0. 35	0. 14	N/A
	H4	1. 38	2. 07	0. 35	0. 14	N/A
	H5	1. 38	2. 07	0. 35	0. 14	N/A
	H6	1. 38	2. 07	0. 35	0. 14	N/A
	H7	1. 38	2. 07	0. 35	0. 14	N/A
	H8	1. 38	2. 07	0. 35	0. 14	N/A
	H9	1. 38	2. 07	0. 35	0. 14	N/A
	H10	1. 38	2. 07	0. 35	0. 14	N/A
	H11	1. 38	2. 07	0. 35	0. 14	N/A
	H12	1. 38	2. 07	0. 35	0. 14	N/A
G and condensers	I1	2. 70	Full (app.) 3. 44	N/A	N/A	N/A
	I2	2. 70	Full (app.) 3. 44	N/A	N/A	N/A
	I3	2. 70	Full (app.) 3. 44	N/A	N/A	N/A
	I4	2. 70	Full (app.) 3. 44	N/A	N/A	N/A
Ejector condenser	J1	Later		N/A	N/A	N/A
	J2			N/A	N/A	N/A
	J3			N/A	N/A	N/A
	J4			N/A	N/A	N/A

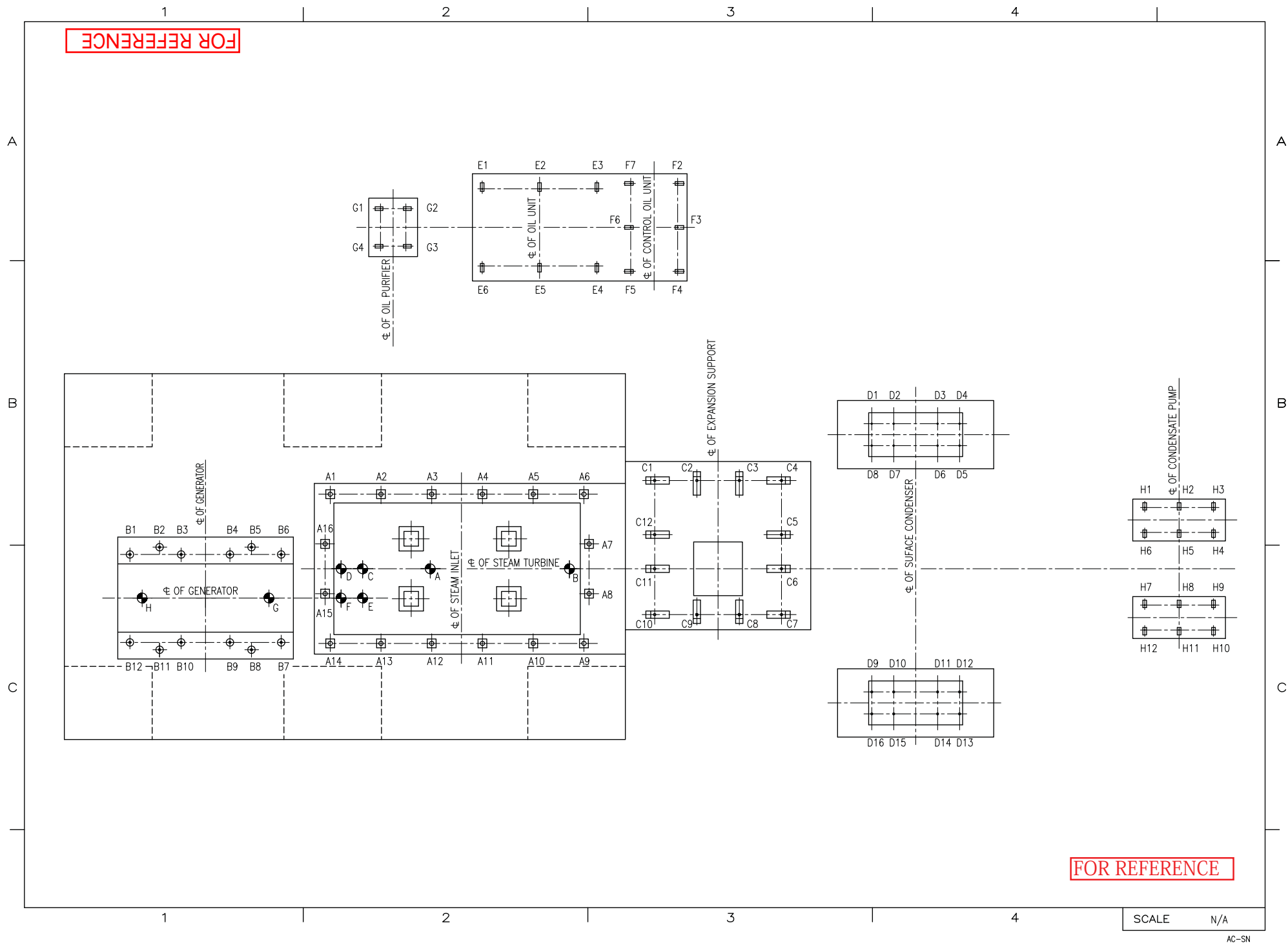
Note: * This Load is included within e.g. piping force and any other conditions not mentioned in this load data.

Unbalance load [kN]

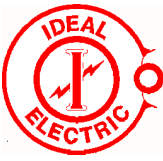
Name	Position		Rotating Weight on Bearing	Unbalance Load
Steam turbine and Reduction gear with base plate	A	Turbine front side	11. 88	2. 02
	B	Turbine rear side	12. 37	2. 10
	C	Reduction gear pinion turbine side	1. 96	0. 34
	D	Reduction gear pinion generator side	1. 96	0. 34
	E	Reduction gear wheel turbine side	14. 21	0. 59
	F	Reduction gear wheel generator side	14. 21	0. 59
Generator	G	Generator front side	60. 27	2. 45
	H	Generator rear side	60. 27	2. 45

Note:

We have not considered weight of Turbine enclosure and Generator roof.
When you design strength calculation of foundation,



44

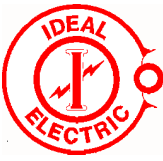


AFTERMARKET SERVICE BULLETIN

GENERAL INSTRUCTIONS FOR ROTOR REMOVAL (SKID PAN METHOD)

Motor or Generator Rotor removal

1. Prepare Site for set up for any associated rigging, timbers, crane and/or gantry as necessary to complete this job.
2. Disconnect and/or lockout all electrical service to the motor. Ensure DE and ODE oil is drained out of the bearing housing. Uncouple the DE from any other unit.
3. Remove the entire exciter assembly from the shaft.
4. Remove the DE and ODE upper and lower bearing bracket covers, if applicable ensure to remove all vibration probe and connections that are mounted on the inner bearing brackets.
5. Remove the DE and ODE upper half bearing brackets. Ensure to remember that the ODE bearing bracket may be insulated from the bearing housing.
6. Remove DE and ODE fan baffles.
7. Remove the DE and ODE upper bearing housing along with the upper bearing half. Inspect the bearing half's for any damage.
8. Remove DE and ODE Bearing temperature probes from the bearing housing.
9. Lift and support the ODE rotor until the lower bearing can be removed from the lower bearing housing. During this process ensure not to lift no more the .010 – .020 inch to allow the bearing to roll. After the lower bearing have has been removed, place G10 blocks spaced apart at 135 degree and 225 degree between the rotor bars and the stator winding iron core (G10 blocks are to be place on the iron core and not the windings) to support the weight of the ODE rotor.
10. Lift and support the DE rotor until the lower bearing can be removed from the lower bearing housing. During this process ensure not to lift no more the .010 – .020 inch to allow the bearing to roll. After the lower bearing have has been removed, place G10 blocks spaced apart at 135 degree and 225 degree between the rotor bars and the stator winding iron core (G10 blocks are to be place on the iron core and not the windings) to support the weight of the DE rotor.
11. Remove ODE and DE lower half bearing bracket.

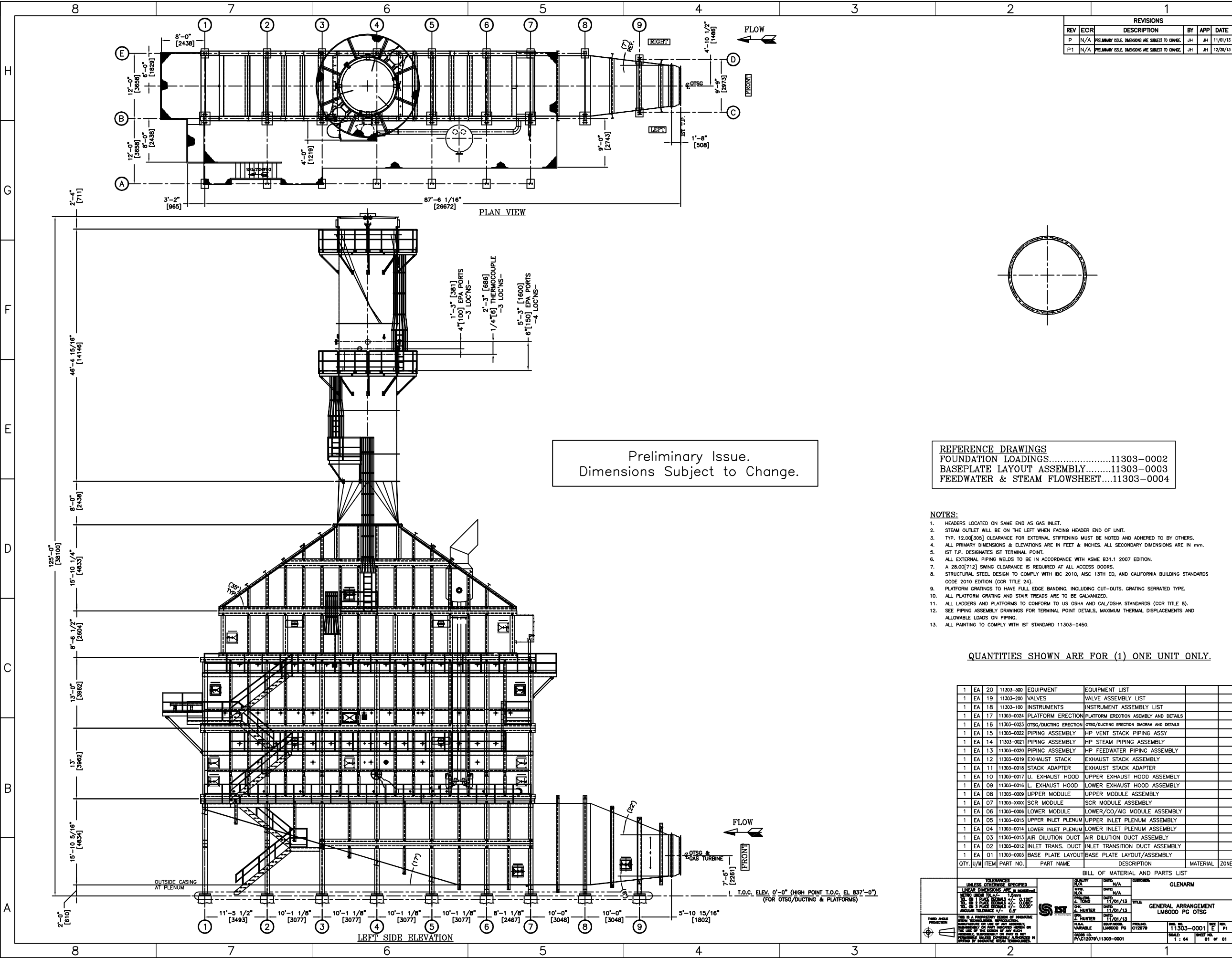


12. Build the necessary cribbing timber up to the bottom of the ODE stator winding iron core. Ensure to place cribbing timber in the ODE stator inboard for skidpan support.
13. Prepare inside surface of skidpan by brushing melted paraffin over entire area.
14. Hoist the ODE rotor up not to exceed the top of the rotor to mesh the top of the stator winding iron core. Remove the G10 block from the ODE, place the skidpan on to the cribbing and slide the skidpan in between the rotor bars and the stator winding iron core until. Let the rotor down to set on the skidpan and repeat the same process for the G10 blocks on the DE.
15. Secure pan with cables and clevises to prevent axial movement
16. Attach a ratchet hoist between the exciter end of the rotor and a substantial anchor point; begin removing rotor out of stator.
17. If lifting means is available, utilize to relieve weight as rotor is removed out of stator.
18. Reassembly is basically the reverse of the above procedure.

Job Notes:

1. Do not substitute other lubricants in place of paraffin.
2. Keep rotor level when removing or reassembling to prevent fan damage.
3. Do not allow skidpan to move in stator.
4. After removing bearings protect journals.
5. Do not lift or pull on journals or other fit surfaces.
6. Before disassembling, for ease of reassembly, establish a reference for shaft extension to determine the approximate axial position of the rotor during assembly.

03-01-08



REVISIONS				
REV	ECR	DESCRIPTION	BY	APP
P	N/A	PRELIMINARY ISSUE. DIMENSIONS ARE SUBJECT TO CHANGE.	JH	JH
P1	N/A	PRELIMINARY ISSUE. DIMENSIONS ARE SUBJECT TO CHANGE.	JH	JH

REFERENCE DRAWINGS
FOUNDATION LOADINGS.....11303-0002
BASEPLATE LAYOUT ASSEMBLY.....11303-0003
FEEDWATER & STEAM FLOWSHEET.....11303-0004

- NOTES:
1. HEADERS LOCATED ON SAME END AS GAS INLET.
 2. STEAM OUTLET WILL BE ON THE LEFT WHEN FACING HEADER END OF UNIT.
 3. TYP. 12.00[305] CLEARANCE FOR EXTERNAL STIFFENING MUST BE NOTED AND ADHERED TO BY OTHERS.
 4. ALL PRIMARY DIMENSIONS & ELEVATIONS ARE IN FEET & INCHES. ALL SECONDARY DIMENSIONS ARE IN mm.
 5. IST T.P. DESIGNATES IST TERMINAL POINT.
 6. ALL EXTERNAL PIPING WELDS TO BE IN ACCORDANCE WITH ASME B31.1 2007 EDITION.
 7. A 28.00[712] SWING CLEARANCE IS REQUIRED AT ALL ACCESS DOORS.
 8. STRUCTURAL STEEL DESIGN TO COMPLY WITH IBC 2010, AISC 13TH ED, AND CALIFORNIA BUILDING STANDARDS CODE 2010 EDITION (CCR TITLE 24).
 9. PLATFORM GRATINGS TO HAVE FULL EDGE BANDING, INCLUDING CUT-OUTS. GRATING SERRATED TYPE.
 10. ALL PLATFORM GRATINGS AND STAIR TREADS ARE TO BE GALVANIZED.
 11. ALL LADDERS AND PLATFORMS TO CONFORM TO US OSHA AND CAL/OSHA STANDARDS (CCR TITLE 8).
 12. SEE PIPING ASSEMBLY DRAWINGS FOR TERMINAL POINT DETAILS, MAXIMUM THERMAL DISPLACEMENTS AND ALLOWABLE LOADS ON PIPING.
 13. ALL PAINTING TO COMPLY WITH IST STANDARD 11303-0450.

QUANTITIES SHOWN ARE FOR (1) ONE UNIT ONLY.

QTY.	U/M	ITEM	PART NO.	PART NAME	DESCRIPTION	MATERIAL	ZONE
1	EA	20	11303-300	EQUIPMENT	EQUIPMENT LIST		
1	EA	19	11303-200	VALVES	VALVE ASSEMBLY LIST		
1	EA	18	11303-100	INSTRUMENTS	INSTRUMENT ASSEMBLY LIST		
1	EA	17	11303-0024	PLATFORM ERECTION	PLATFORM ERECTION ASSEMBLY AND DETAILS		
1	EA	16	11303-0023	OTSG/DUCTING ERECTION	OTSG/DUCTING ERECTION DIAGRAM AND DETAILS		
1	EA	15	11303-0022	PIPING ASSEMBLY	HP VENT STACK PIPING ASSY		
1	EA	14	11303-0021	PIPING ASSEMBLY	HP STEAM PIPING ASSEMBLY		
1	EA	13	11303-0020	PIPING ASSEMBLY	HP FEEDWATER PIPING ASSEMBLY		
1	EA	12	11303-0019	EXHAUST STACK	EXHAUST STACK ASSEMBLY		
1	EA	11	11303-0018	STACK ADAPTER	EXHAUST STACK ADAPTER		
1	EA	10	11303-0017	U. EXHAUST HOOD	UPPER EXHAUST HOOD ASSEMBLY		
1	EA	09	11303-0016	L. EXHAUST HOOD	LOWER EXHAUST HOOD ASSEMBLY		
1	EA	08	11303-0009	UPPER MODULE	UPPER MODULE ASSEMBLY		
1	EA	07	11303-0001	SCR MODULE	SCR MODULE ASSEMBLY		
1	EA	06	11303-0008	LOWER MODULE	LOWER/CO/AIG MODULE ASSEMBLY		
1	EA	05	11303-0015	UPPER INLET PLENUM	UPPER INLET PLENUM ASSEMBLY		
1	EA	04	11303-0014	LOWER INLET PLENUM	LOWER INLET PLENUM ASSEMBLY		
1	EA	03	11303-0013	AIR DILUTION DUCT	AIR DILUTION DUCT ASSEMBLY		
1	EA	02	11303-0012	INLET TRANS. DUCT	INLET TRANSITION DUCT ASSEMBLY		
1	EA	01	11303-0003	BASE PLATE LAYOUT	BASE PLATE LAYOUT/ASSEMBLY		

UNLESS OTHERWISE SPECIFIED
LINEAR DIMENSIONS ARE IN INCHES
ANGULAR DIMENSIONS ARE IN DEGREES
TOL. ON 1 PLACE DECIMALS +/- 0.125"
TOL. ON 2 PLACE DECIMALS +/- 0.0625"
TOL. ON 3 PLACE DECIMALS +/- 0.03125"
ANGULAR TOLERANCE +/- 0.5°

THIS IS A PRELIMINARY DESIGN OF A MACHINE
AND SHOULD NOT BE USED FOR CONSTRUCTION
OR FOR THE DESIGN OF ANY PARTS OR
COMPONENTS. IT IS NOT TO BE USED FOR
CONSTRUCTION OR FOR THE DESIGN OF ANY
PARTS OR COMPONENTS. IT IS NOT TO BE
USED FOR CONSTRUCTION OR FOR THE DESIGN
OF ANY PARTS OR COMPONENTS.

QUALITY
N/A
DATE
N/A

DESIGN
N/A
DATE
N/A

ENGINEER
N/A
DATE
N/A

IN CHARGE
N/A
DATE
N/A

WARRANTY
N/A
DATE
N/A

OWNER
N/A
DATE
N/A

DATE
11/01/13

DATE
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DATE
11/01/13

DATE
11/01/13

REVISIONS

11303-0001

11303-0001

11303-0001

11303-0001

11303-0001

11303-0001

GLENARM

GENERAL ARRANGEMENT

LM8000 PG OTSG

SCALE 1" = 6'

SHEET 01 OF 01